

CHAPTER - 5

## INTRODUCTION

### Review of earlier works

The majority of reactions that are of chemical or biological in nature occur in solution. It was previously believed that solvent merely provides an inert medium for chemical reactions. The significance of solute-solvent interactions was realised only recently as a result of extensive studies in aqueous, non-aqueous and mixed solvents<sup>1-10</sup>.

Water is the most abundant solvent in nature. In view of its extreme importance to chemistry, biology, agriculture, geology, etc., water has been extensively used in kinetic and equilibrium studies. In spite of such extensive studies, our knowledge of molecular interactions in water is extremely limited. Moreover, the uniqueness of water as solvent has been questioned<sup>11, 12</sup> in recent years and it has been realised that the studies in other solvent media (non-aqueous and mixed solvents) would be of great help in understanding different molecular interactions and a host of complicated phenomena<sup>1-10</sup>.

Extensive studies on the physical properties of different solvent systems have been made but a lacunary gap still exists. Several classifications of organic solvent systems based on their dielectric constants, organic group type, acid-

base properties or association through hydrogen bonding<sup>10</sup>,  
donor-acceptor-properties<sup>13</sup>, hard and soft acid-base principles<sup>14</sup> etc. have been used; the different solvent systems show a wide divergence of properties which would naturally be reflected on the thermodynamic and transport properties of electrolytes and non-electrolytes in these solvents. The determination of thermodynamic and transport properties of different electrolytes in various solvents would thus provide an important step in this direction. Naturally, in the development of theories dealing with electrolyte solutions, much attention has been devoted to ion-solvent interactions which are "controlling forces" in infinitely dilute solutions where ion-ion interactions are absent. Ion-solvent interactions or broadly solute-solvent interactions are important in understanding the physico-chemical properties of solutions. It is very difficult to suggest the forces or factors involved in the solute - (or ion) solvent interactions as most of their determining factors remain obscure. Ion-solvent (or solute-solvent) interactions manifest themselves in all thermodynamic and transport properties of electrolytes generally obtained by extrapolation to infinite dilution. By separating these functions into ionic contributions, it is possible to determine the contributions due to cations and anions in the solute-solvent interactions. These depend on the intrinsic solvent

structure and on the nature of the ions (dimension, charge, charge distribution in case of large ions, H-bonding etc.).

One of the reasons for the intricacies in solution chemistry is that the structure of the solvent molecules is not known with certainty. The introduction of an ion or solute modifies the solvent structure to an uncertain magnitude whereas the solute molecules are also modified and the interplay of forces like solute-solute, solute-solvent and solvent-solvent interactions becomes predominant though the isolated picture of any of them is not known with certainty.

The problem of ion-solvent interactions which are closely akin to ionic solvation can be studied from different angles using almost all the available physico-chemical techniques.

Ion-solvent interactions can be studied spectroscopically : the spectral solvent shifts or the chemical shifts determine their qualitative and quantitative nature. But even qualitative or quantitative apportioning of the ion-solvent interactions into the various possible factors is still <sup>an</sup> uphill task.

The ion-solvent interactions can also be studied from the thermodynamic point of view where changes of the free energy, enthalpy and entropy etc. associated with a particular

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reaction can be qualitatively and quantitatively evaluated (using various physico-chemical techniques) from which conclusions regarding the factors associated with the ion-solvent interactions can be worked out.

Similarly, the ion-solvent interactions can be studied using solvational approaches involving the studies of different properties such as viscosity, conductance and compressibility etc. of electrolytes and derive the various factors associated with ionic solvation.

We shall particularly dwell upon the different aspects of these transport properties as the present dissertation is intimately related to the studies of viscosities and conductances of different tetraalkyl ammonium bromides and alkali metal halides (chlorides and bromides) in 'quasi-protic' solvent, 2-Methoxy Ethanol (ME) and its binary aqueous mixtures and in aprotic solvent, i.e. 1,2-Dimethoxy Ethane (DME).

### Viscosity

Viscosity is one of the most important transport properties used for the determination of ion-solvent interactions and studied extensively<sup>13,16</sup>. Viscosity is not a thermodynamic quantity, but viscosity of an electrolytic solution together with thermodynamic property  $\bar{V}_2$ , partial molar volume, gives much information and insight regarding ion-solvent interactions.

and the structures of the electrolytic solutions. The viscosity relationships of electrolytic solutions are highly complicated. There are strong electrical forces between the ions and solvent, and separation of the forces is not really possible. But from careful analysis, valid conclusions can be drawn regarding the structure and the nature of the solvation of the particular system.

The viscosity is a measure of the friction between adjacent, relatively moving parallel planes of the liquid. Anything that increases or decreases the interaction between the planes will raise or lower the friction and therefore, increase or decrease the viscosity.

If large spheres are placed in the liquid, the planes will be keyed together in increasing the viscosity. Similarly, increase in the average degree of hydrogen-bonding between the planes will increase the friction between the planes, thereby viscosity. An ion with a large rigid co-sphere (for a structure promoting ion) will behave as a rigid sphere placed in the liquid and increase the inter planar friction. Similarly, an ion increasing the degree of hydrogen bonding or the degree of correlation among the adjacent solvent molecules, will increase the viscosity. Conversely, ions destroying correlation would decrease the viscosity. The <sup>coulomb</sup> interaction of the ions also keys the plane together and gives a  $c^2$  dependence

on concentration, but the effect is small and will be swamped at moderate temperatures.<sup>16</sup>

The first systematic measurements of viscosities of a number of electrolyte solutions over a wide concentration range was attempted by Grünisen<sup>17</sup> in 1905. He noted non-linearity and negative curvature in the viscosity concentration curves (irrespective of low or high concentrations). In 1929, Jones and Dole<sup>18</sup> suggested an empirical equation (1), quantitatively correlating the relative viscosities of the electrolytes with molar concentrations C.

$$\frac{\eta}{\eta_0} = 1 + AC^{\frac{1}{2}} + BC \quad \dots (1)$$

The equation reduces to

$$(\eta/\eta_0 - 1)/C^{\frac{1}{2}} = A + BC^{\frac{1}{2}} \quad \dots (2)$$

where A and B are constants specific to ion and the solvent. The equation is applicable equally to aqueous and non-aqueous solvent systems and used extensively. The term  $AC^{\frac{1}{2}}$ , originally ascribed to Grünisen effect, arose from the long range coulomb forces between the ions. The significance of the term had since then been realized due to the development of Debye-Hückel theory<sup>19</sup> of inter ionic attractions (1923), Falkenhagen's<sup>20-22</sup> theoretical calculation of the constant 'A', using the equilibrium theory and the theory of irreversible processes. An

electrolytes developed by Onsager and Fuoss<sup>23</sup>. The A-coefficient depends on the ion-ion interactions and can be calculated from the physical properties of solvent and solution using the Gahlenhagen-Vernon<sup>22</sup> equation

$$A_{\text{theor}} = \frac{0.2577 \Lambda^0}{\eta_0 (\epsilon T)^{1/2} \lambda_+^0 \lambda_-^0} \left[ 1 - 0.6863 \left( \frac{\lambda_+^0 - \lambda_-^0}{\Lambda^0} \right)^2 \right] \dots (3)$$

where  $\Lambda^0$ ,  $\lambda_+^0$  and  $\lambda_-^0$  are the limiting conductances of the electrolyte and the ions respectively at temperature T. and  $\eta_0$  are the dielectric constant and viscosity of the solvent. For most solutions, both aqueous and non-aqueous, the equation is valid upto 0.1M<sup>19,24</sup>. At higher concentrations, the extended Jones-Pople equation (4) involving an additional constant D, originally used by Kandulsky<sup>25</sup> has been used by several workers<sup>26,27</sup>.

$$\frac{\eta}{\eta_0} = 1 + AC^2 + BC + DC^2 \dots (4)$$

The constant D cannot be evaluated properly and the significance of the constant is also not always meaningful and therefore, the equation (1) is used by most of the workers.

The plots of  $(\eta/\eta_0 - 1)C^2$  against  $C^2$  for the electrolytes should give the value of A but in general the values come out to be negative or considerably scatter and deviation from linearity occur<sup>24,26,29</sup>. Thus, instead of determining A-values

from the plots or by least square method, the A-values are generally calculated using Falkenhagen-Vernon equation (3).

A-coefficient should be zero for non-electrolytes. According to Jones and Dole, the co-efficient, A, probably represents the stiffening effect on the solution of the electric forces between the ions which tend to maintain a space-lattice structure<sup>18</sup>.

The B-coefficient may be either positive or negative and it is actually the ion-solvent interaction parameter. It is conditioned by the ion-size and the solvent and cannot be calculated a priori. The B-coefficients are obtained as slopes of the straight lines using the least square method and intercepts equal to the A-values. The factors which increase or decrease the viscosities of the solvent as enumerated at the beginning also condition the increase or decrease of B-values. The factors which influence B-values are<sup>30,31</sup>:

(1) The effect of ionic solvation and the action of the field of the ion in producing long range order in solvent molecules increase  $\eta$  or B-values.

(2) The destruction of the three dimensional structure of solvent molecules (i.e. structure breaking effect or depolymerization effect) decrease  $\eta$  -values.

(3) High molar volume and low dielectric constant yield high B-values for similar solvents.

(4) Reduced  $\eta_{sp}$ -values are obtained when the primary solvation of ions is sterically hindered in high molal volume solvents or if either ion of a binary electrolyte cannot be specifically solvated.

Viscosities at higher concentrations:

It had been found that the viscosity values at high concentrations (1M to saturation) can be represented by the empirical formula suggested by Andrade<sup>32</sup>

$$\eta = A \exp b/T \quad \dots (5)$$

Several alternative formulations have been proposed for representing the results of viscosity measurements in the high concentration range<sup>33-38</sup> and the equation suggested by Angell<sup>39,40</sup> based on an extension of the free volume theory of transport phenomena in liquids and fused salts to ionic solutions is particularly noteworthy.

The equation is

$$1/\eta = A \exp \left[ - \frac{K'}{N_0 - N} \right] \quad \dots (6)$$

where  $N$  represents the concentration of the salt in eqv.  
litres<sup>-1</sup>,  $A$  and  $K'$  are constant supposed to be independent of  
the salt composition and  $N_0$  is the hypothetical concentration  
at which the system becomes glass. The equation was recast by

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Majumdar et al introducing the limiting condition that as  $N \rightarrow 0$ ,  $\eta \rightarrow \eta_0$ , the viscosity of the pure solvent. Thus, we have

$$\ln \frac{\eta}{\eta_0} = \ln \eta_{\text{rel}} = \frac{K'N}{N_0(N_0 - N)} \quad \dots (7)$$

The equation (7) predicts a straight line passing through the origin for the plot of  $\ln \eta_{\text{rel}}$  vs  $N/(N_0 - N)$ , if a suitable choice for  $N_0$  is made. The equation (7) has been tested by Majumdar et al using the data from the literature and from their own experimental results. The best choice for  $N_0$  and  $K'$  was selected by a trial and error method. The set of  $K'$  and  $N_0$  which produce minimum deviation between  $\eta_{\text{rel}}$  (expt) and  $\eta_{\text{rel}}$  (theo) was accepted.

In dilute solutions,  $N \ll N_0$  and we have

$$\eta_{\text{rel}} = \exp(K'N/N_0^2) \approx 1 + \frac{K'N}{N_0^2} \quad \dots (8)$$

which is nothing but the Jones-Dole equation with the ion-ion interaction term represented as  $B = \frac{K'}{N_0^2}$ . The arrangement between  $B$  values determined in this way and using Jones-Dole equation has been found to be good for several electrolytes.

Further the equation (7) written in the form

$$\frac{N}{\ln \eta_{\text{rel}}} = \frac{N_0^2}{K'} = \frac{N_0^2}{K'} B \quad \dots (9)$$

closely resembles Vand's equation<sup>36</sup> for fluidity (reciprocal for viscosity):

$$\frac{2.5}{2.3 \log \eta_{\text{rel}}} = \frac{1}{V} - Qc \quad \dots (10)$$

where C is the molar concentration of the solute and V is the effective rigid molar volume of the salt and Q is the interaction constant.

#### Division of B Co-efficient into ionic values

The viscosity B-coefficients have been determined by a large number of workers in aqueous, mixed and non-aqueous solvents<sup>29,44-74</sup>. However, the B-coefficients as determined experimentally using Jones-Dole equation, does not give any impression regarding ion-solvent interactions unless there is some way to identify the separate contributions of cations and anions in the total solute-solvent interactions. It is well known that no physico-chemical property of the total solute can reflect the properties of the individual ions and only ionic contributions may give insight on the intrinsic nature of the solvent structure and its modification by the ions (conditioned by the dimension, charge, charge distribution, H-bonding etc.). The division of B-values into ionic B<sup>+</sup> and B<sup>-</sup> values is quite arbitrary based on some approximation or

assumptions, the validity of which may be questioned.

The following methods have been used for the division of B-values into ionic components:

(1) Cox and Wolfenden<sup>75</sup> carried out the division on the assumption that B<sub>ion</sub> values of Li<sup>+</sup> and SO<sub>4</sub><sup>2-</sup> in LiClO<sub>4</sub> are proportional to the ionic volumes which are proportional to the third power of the ionic mobilities. The method of Gurney and also of Kaminsky<sup>25</sup> is based on

$$B_{K^+} = B_{Cl^-} \text{ (in Water)} \quad \dots (11)$$

The argument in favour of this assignment is based on the fact that the B-coefficient for KCl is very small and that the mobilities of K<sup>+</sup> and Cl<sup>-</sup> are very similar over the temperature range 15-45° C. The assignment is supported from other thermodynamic properties<sup>15</sup>. Nightingale<sup>77</sup>, however, preferred NaCl or CsCl rather than KCl from stability considerations.

(2) The method suggested by Desoyern and Perron<sup>26</sup> is based on the assumption that the ion Hg<sub>2</sub>H<sup>+</sup> in water is probably closest to being neither structure breaker nor a structure maker. Thus they suggest that it is possible to apply with a high degree of accuracy, Einstein's equation<sup>78</sup>

$$B = 0.0025 \bar{V}_o \quad \dots (12)$$

and by having accurate values of the partial molar volume of the ion  $\bar{V}_o$  it is possible to calculate the value of 0.359 for  $B_{Et_3N^+}$  in water at 25°C.

Recently Sacco et al.<sup>69</sup> proposed the widely used "reference electrolyte" method. Thus for tetraphenyl phosphonium tetraphenyl borate in water, we have

$$B_{Ph_4^-} = B_{Ph_4^+} = B_{Ph_4PPh_4}/2 \quad \dots (13)$$

$B_{Ph_4PPh_4}$  (scarcely soluble in water) is obtained for

$$B_{Ph_4^+} + B_{PPh_4Br} = B_{Na^+} = B_{Ph_4PPh_4} \quad \dots (14)$$

the values obtained are in good agreement with those obtained by other methods.

The criteria adopted for the separation of B-coefficients in non-aqueous solvents differ from those generally used in water. However, the methods are based on the equality of equivalent conductances of counter ions at infinite dilutions. Thus,

(a) Criss and Mastrianni<sup>47</sup> assumed  $B_{K^+} = B_{Cl^-}$  in methanol (based on equal mobilities of ions<sup>79</sup>). They also adopted  $B_{Ph_4^+} = 0.25$  as the initial value for acetonitrile solutions.

(b) For acetonitrile solutions, Tuan and Fuoss<sup>80</sup> proposed the equality

$B_{Bu_4N^+} = B_{Ph_4B^-}$  ... (15), since they thought that these ions have similar mobilities. However, according to Springer et al.,  $\lambda_0^{25} \cdot Bu_4N^+ = 61.4$  and  $\lambda_0^{25} \cdot Ph_4B^- = 58.3$  in acetonitrile.

(c) Gopal and Restogi<sup>45</sup> resolved the B-coefficient in N-methyl propionamide solutions, assuming (without proof) that

$B_{Et_4N^+} = B_{x^-}$  ... (16) at all temperatures. In dimethylsulphoxide, the division of B-coefficients were carried out by Yeo and Bennion<sup>28</sup> assuming  $B[(i-pe)_3BuN^+] = B[Ph_4B^-] = 1/2 B[(i-pe)_3BuNPh_4B^-]$  ... (17) at all temperatures.

Wide use of this method has been made by other authors for dimethylsulphoxide<sup>27</sup>, sulphone<sup>55</sup>, hexamethylphosphotriamide<sup>59</sup> and ethylene carbonate<sup>82</sup> solutions.

The methods, however, have been strongly criticized by Krugatz<sup>83</sup>. According to him, any method of resolution based on the equality of equivalent conductance for certain ion buffers from the drawback that it is impossible to select any two ions for which  $\Lambda_{o,+} = \Lambda_{o,-}$  in all solvents at proper temperatures. Thus, though  $\Lambda_o K^+ = \Lambda_o Cl^-$  at 25°C in methanol, but not in ethanol or in other solvents. In addition, if the mobilities of some ions are even equal at infinite dilution, but it is not necessarily true at moderate concentrations for which the B-coefficient values are calculated. Further, according to him, equality of dimensions of  $(i-pe)_3BuN^+$  or  $(i-am)_3BuN^+$  and  $Ph_4B^-$  does not necessarily imply equality of B-coefficients of these ions and they are likely to be solvent and ion-structure dependent.

Brunzaik<sup>63, 64</sup> has recently proposed a method for the resolution of B-coefficients. The method is based on the fact that the large tetraalkylammonium cations<sup>65, 66</sup> are not solvated in organic solvents (in the normal sense involving significant electrostatic interaction). Thus, the ionic B-values for large tetraalkylammonium ions  $R_4N^+$  (where R > Bu) in organic solvents are proportional to their ionic dimensions.

Thus we have

$$B_{R_4NX} = a + b \frac{r^3}{R_4N^+} \quad \dots (18)$$

where  $a = B_{X^-}$  and b is a constant dependent on temperature and solvent nature.

The extrapolation of the plot of  $B_{R_4NX}$  (R > Pr or Bu) against  $r^3_{R_4N^+}$  to zero cation dimension gives directly  $B_{X^-}$ . In the proper solvent from which other B-ion values can be calculated.

The B-ion values can also be calculated from the equations

$$B_{R_4N^+} = B_{R_4H^+} = B_{R_4NX} - B_{R_4HX} \quad \dots (19)$$

and

$$\frac{B_{R_4N^+}}{B_{R_4H^+}} = \frac{r^3_{R_4N^+}}{r^3_{R_4H^+}} \quad \dots (20)$$

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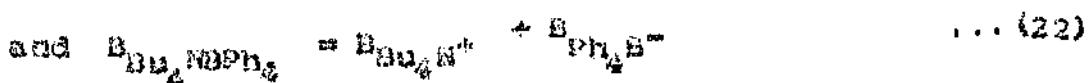
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The radii of the tetraalkylammonium ion have calculated from the accurate conductometric data<sup>37</sup>.

Gill and Sharma<sup>70</sup> used  $\text{Bu}_4\text{N}^+$  as a reference electrolyte. The method of resolution of S is based on the assumption, like Krungatz that  $\text{Bu}_4\text{N}^+$  and  $\text{Ph}_4\text{B}^-$  ions with large R-groups are not solvated in non-aqueous solvents and their dimensions in such solvents are constant. The ionic radii of  $\text{Bu}_4\text{N}^+$  ( $5.00 \text{ \AA}^0$ ) and  $\text{Ph}_4\text{B}^-$  ( $5.35 \text{ \AA}^0$ ) have, in fact, found to remain constant in different non-aqueous and mixed non-aqueous solvents by Gill and co-workers. They proposed the equations

$$\frac{s_{\text{Ph}_4\text{B}^-}}{s_{\text{Bu}_4\text{N}^+}} = \frac{r_{\text{Ph}_4\text{B}^-}^3}{r_{\text{Bu}_4\text{N}^+}^3} = \left(\frac{5.35}{5.00}\right)^3 \dots (21)$$



The method requires only the S-values of  $\text{Bu}_4\text{N}^+$  and is equally applicable to mixed non-aqueous solvents. The B-ion values obtained by this method agree well with those reported by Sacco et al in different organic solvents using assumption :

$$s_{\text{Li}-\text{Am}_3\text{Bu}_4\text{N}^+} = s_{\text{Ph}_4\text{B}^-} = s_{\text{Li}-\text{Am}_3\text{Bu}_4\text{N}^+\text{Ph}_4\text{B}^-}/2 \dots (23)$$

Recently Lawrence and Sacco<sup>71, 72a</sup> used (tetrabutylammonium tetrabutyl borate)  $\text{Bu}_4\text{N}^+\text{Bu}_4\text{B}^-$  and tetraphenyl phosphonium tetraphenyl borate ( $\text{Ph}_4\text{P}^+\text{Ph}_4\text{B}^-$ ) as reference electrolytes because the cation and anion in each case are symmetrically shaped and have almost equal van der Waals volumes.

Thus, we have,

$$\frac{B(\text{Bu}_4\text{N}^+)}{B(\text{Bu}_4\text{B}^-)} = \frac{v_p(\text{Bu}_4\text{N}^+)}{v_p(\text{Bu}_4\text{B}^-)} \quad \dots (24)$$

$$\text{or } B(\text{Bu}_4\text{N}^+) = B(\text{Bu}_4\text{N}^+\text{Bu}_4\text{B}^-) / \left[ 1 + \frac{v_p(\text{Bu}_4\text{N}^+)}{v_p(\text{Bu}_4\text{B}^-)} \right] \quad \dots (25)$$

A similar division can be made for the  $\text{Ph}_4\text{P}^+\text{Ph}_4\text{B}^-$  system. Recently, Lawrence et al.<sup>72b</sup> determined the viscosity measurement of tetralkyl (from Pr to Nept) ammonium bromides in DMSO and HMPA.

The B coefficients

$$B(\text{R}_4\text{N}^+) = B(\text{Br}^-) = a \left[ f_x(\text{R}_4\text{N}^+) \right]$$

were plotted as functions of the van der Waals volumes. Stokes radii and formula weight of the cations to get  $B(\text{Br}^-)$  value. The  $B(\text{Br}^-)$  values thus obtained were compared with the accurately determined  $B(\text{Br}^-)$  value obtained using  $\text{Bu}_4\text{N}^+\text{Bu}_4\text{B}^-$  and  $\text{Ph}_4\text{P}^+\text{Ph}_4\text{B}^-$  as reference salts. They concluded that the 'reference salt' method

is the best available method for the division into ionic contributions. Their analysis is in agreement with the conclusions made by Thomson et al.<sup>72c,d</sup>.

Jenkins and Pritchett<sup>88</sup> suggested a least square analytical technique to examine additivity relationship for combined ion thermodynamics data, to effect apportioning into single-ion components for alkali metal halide salts by employing Rajans' competition principle<sup>99</sup> and 'Volcano plots' of Morris<sup>90</sup>. The principle was extended to derive absolute single ion B-coefficients for alkali metals and halides in water. They also observed that  $B(\text{Cs}^+) \approx B(\text{I}^-)$  suggested by Kruygalz<sup>85</sup> to be more reliable than  $B(\text{K}^+) = B(\text{Cl}^-)$  in aqueous solutions. However, we require more data to test the validity of this method.

It is apparent that most of these methods are based on certain approximations and anomalous results may arise unless proper mathematical theory is developed to calculate B-values.

#### Temperature dependence of $B_{\text{ion}}$ - Values:

A regularity in the behaviour of  $B_{\pm}$  and  $\partial B_{\pm} / \partial T$  has been observed both in aqueous and non-aqueous solvents<sup>15</sup> and useful generalizations have been made by Kaminsky<sup>25</sup>. He observed that (1) within a group of the periodic table the b-ion values decrease as the crystal ionic radii increase.

(ii) Within a group of periodic system, the temperature coefficient of  $B_{ion}$  values increases as the ionic radius increases. The results can be summarized as follows:

$$(i) B < 0 \text{ and } \frac{dB}{dT} > 0 \quad \dots (26)$$

$$(ii) B_{ion} < 0 \text{ and } \frac{dB_{ion}}{dT} > 0 \quad \dots (27)$$

characteristic of structure breaking ions.

$$(iii) B_{ion} > 0 \text{ and } \frac{dB_{ion}}{dT} < 0,$$

characteristic of structure making ions ... (28)

It is well known that an ion is surrounded by a solvation sheath and the properties of the solvents which are different from those present in the bulk structure. This is well reflected in the 'co-sphere' model of Gurney<sup>91</sup>, A,B,C zones of Frank and Wen<sup>92</sup> and hydrated radius of Nightingale<sup>77</sup>.

Stokes and Mills<sup>15</sup> gave an analysis of viscosity incorporating the basic ideas presented before. The viscosity of a dilute electrolyte solution has been equated to the viscosity of the solvent ( $\eta_0$ ) plus the viscosity changes resulting from competition between various effects occurring in the ionic neighbourhood. Thus,

$$\eta = \eta_0 + \eta^* + \eta^E + \eta^A + \eta^D = \eta_0 + \eta_0 (A\bar{c} + Bc) \quad \dots (29)$$

(Jones-Sole equation)

$\eta^*$  is the positive increment in viscosity caused by coulombic interaction. Thus,

$$\eta^E + \eta^A + \eta^D = \eta_{\text{BC}} \quad \dots (30)$$

B-coefficient can thus be interpreted in terms of competitive viscosity effects.

Following Stokes and Mills<sup>15</sup> and Krungatz<sup>83</sup> we can write for  $B_{\text{ion}}$

$$B_{\text{ion}} = B_{\text{ion}}^{\text{inst}} + B_{\text{ion}}^{\text{orient}} + B_{\text{ion}}^{\text{str}} + B_{\text{ion}}^{\text{reinf}} \quad \dots (31)$$

whereas according to Lawrence and Sacco<sup>71</sup>,

$$B_{\text{ion}} = B_{\text{ij}} + B_{\text{Solv}} + B_{\text{shape}} + B_{\text{ord}} + B_{\text{discord}} \quad \dots (32)$$

$B_{\text{ion}}^{\text{inst}}$  is the positive increment arising from the obstruction to the viscous flow of the solvent caused by the shape and size of the ions (the term corresponds to  $\eta^*$  or  $B_{\text{shape}}$ ),  $B_{\text{ion}}^{\text{orient}}$  is the positive increment arising from the alignment or structure-making action of the electric field of the ion on the dipoles of the solvent molecules (the term corresponds to  $\eta^A$  or  $B_{\text{ord}}$ ).  $B_{\text{ion}}^{\text{str}}$  is the negative increment related to the destruction of the solvent structure in the region of ionic co-sphere arising from the opposing tendencies of the ion to orientate the molecules round itself censrosymmetrally and

solvent to keep its own structure. (This corresponds to or  $B_{\text{discord}}$ ).

$B_{\text{ion}}^{\text{reinf}}$  is the positive increment conditioned by the effect of 'reinforcement of the water structure' by large tetraalkylammonium ions due to hydrophobic hydration. The phenomenon is inherent in the intrinsic water structure and absent in organic solvents.

$B_w$  and  $B_{\text{solv}}$  account for viscosity increases attributed to the vander Waals volume and the volume of the solvation of ions.

Thus, small and highly charged cations like  $\text{Li}^+$  and  $\text{Mg}^{2+}$  form a firmly attached primary solvation sheath around these ions ( $B_{\text{inst}}$  or  $\eta^{\beta}$  positive).

At ordinary temperatures, alignment of the solvent molecules around the inner layer also cause increase in  $B_{\text{orient}}$  ( $\eta^A$ ),  $B_{\text{ion}}^{\text{str}}$  ( $\eta^B$ ) is small for these ions.

Thus  $B_{\text{ion}}$  will be large and positive as  $B_{\text{ion}}^{\text{inst}} > B_{\text{ion}}^{\text{orient}} > B_{\text{ion}}^{\text{str}}$ . However,  $B_{\text{ion}}^{\text{inst}}$  and  $B_{\text{ion}}^{\text{orient}}$  would be small for ions of greatest crystal radii (within a group) like  $\text{Cs}^+$  or  $\text{I}^-$  due to small surface charge densities resulting in weak orienting and structure forming effect.  $B_{\text{ion}}^{\text{str}}$  would be large due to structural disorder in the immediate neighbourhood of the ion due to competition between the ionic field and the bulk structure.

thus  $B_{\text{ion}} + B_{\text{ion}}^{\text{Orient}} < B_{\text{ion}}$  and  $B_{\text{ion}}$  is negative.

Ions of intermediate size (e.g.  $\text{K}^+$  and  $\text{Cl}^-$ ) have a close balance of viscous forces in their vicinity, i.e.  $B_{\text{ion}} + B_{\text{ion}}^{\text{Orient}} = B_{\text{ion}}^{\text{Str}}$  so that  $B$  is close to zero.

Large molecular ions like tetramethylammonium ions have large  $B_{\text{ion}}$  because of large size but  $B_{\text{ion}}^{\text{Orient}}$  and  $B_{\text{ion}}^{\text{Str}}$  would be small i.e.  $B_{\text{ion}} + B_{\text{ion}}^{\text{Orient}} + B_{\text{ion}}^{\text{Str}}$  and  $B$  would be positive and large. The value would be further reinforced in water arising from  $B_{\text{ion}}^{\text{reinf}}$  due to hydrophobic hydrations.

The increase in temperature will have no effect on  $B_{\text{ion}}^{\text{Orient}}$  but the orientation of solvent molecules in the secondary layer will be decreased due to increase thermal motion leading to decrease in  $B_{\text{ion}} + B_{\text{ion}}^{\text{Orient}}$ .  $B_{\text{ion}}^{\text{Str}}$  will decrease slowly with temperature as there will be less competition between the ionic field and the reduced solvent structure. The positive or negative temperature coefficient will thus depend on the change of the relative magnitudes of  $B_{\text{ion}}^{\text{Orient}}$  and  $B_{\text{ion}}^{\text{Str}}$ .

It is clear that in case of structure-making ions, the ions are firmly surrounded by a primary solvation sheath and the secondary solvation zone will be considerably ordered leading to an increase in  $B_{\text{ion}}$  and concomitant decrease in entropy of solvation and the mobility of ions. Structure-breaking ions, on the other hand, are not solvated to a great extent and the secondary solvation zone will be disordered leading to a

decrease in  $B_{ion}$  values and increase in entropy solvation and the mobility of ions. Moreover, the temperature induced change in viscosity of ions (or entropy of solvation or mobility of ions) would be more pronounced in case of smaller ions than in case of the larger ions. So there is a clear correlation between the viscosity, entropy of solvation and temperature dependent mobility of ions. Thus, the ionic B-coefficients and entropy of solvation of ions have rightly been used as probes of ion-solvent interactions and as a direct indication of structure - making and structure-breaking characters of ions.

The linear plot of ionic B-coefficients against the ratios of mobility-viscosity products at two temperature (a more sensitive variable than ionic mobility) by Gurney<sup>75,91</sup> clearly demonstrates a close relation between ionic B-coefficients and ionic mobilities.

Gurney also demonstrated a clear correlation between the molar entropy of solution values with B-coefficient of salts. The ionic B-values show a linear relationship with the partial molar ionic entropies of hydration  $\bar{s}_h^\circ$ .

$$\bar{s}_h^\circ = \bar{s}_{aq}^\circ = \bar{s}_g^\circ \quad \dots (33)$$

where  $\bar{s}_{aq}^\circ = \bar{s}_{ref}^\circ + \Delta s^\circ$ ,  $\bar{s}_g^\circ$  is the calculated sum of the translational and rotational entropies of the gaseous ions.

Gurney obtained a single linear plot between ionic entropies

and ionic B coefficients for all monoatomic ions by equating the entropy of the hydrogen ion ( $S_{H^+}^{\circ}$ ) to  $-5.5 \text{ cal mole}^{-1}\text{deg}^{-1}$ .

Hamus<sup>93</sup> used the entropy of hydration to correlate ionic B-values and Nightingale<sup>77</sup> showed that a single linear relationship can be obtained with it for both monoatomic and polyatomic ions.

The correlation was utilised by Abraham et al.<sup>24</sup> to assign single-ion B-coefficients so that a plot of  $\Delta S_e^{\circ}$ <sup>93,96</sup>, the electrostatic entropy of solvation or  $\Delta S_{I,II}^{\circ}$ <sup>93,98</sup>, the entropic contributions of the first and second solvation layers, of ions against B points (taken from the works of Nightingale) for both cations and anions lie on the same curve or line. There are excellent linear correlations between  $\Delta S_e^{\circ}$  and  $\Delta S_{I,II}^{\circ}$ , and the single ion B-coefficients. Both entropy criteria ( $\Delta S_e^{\circ}$  and  $\Delta S_{I,II}^{\circ}$ ) and B-ion values indicate that in water the ions  $\text{Li}^+$ ,  $\text{Na}^+$ ,  $\text{Ag}^+$  and  $\text{F}^-$  are net structure-makers the ions  $\text{Nb}^+$ ,  $\text{Cs}^+$ ,  $\text{Cl}^-$ ,  $\text{Br}^-$ ,  $\text{I}^-$  and  $\text{ClO}_4^-$  are structure-breakers and  $\text{K}^+$  is a border line case. In non-aqueous solvents formamide, methanol, *n*-methyl formamide, dimethyl formamide, dimethyl sulphoxide and acetonitrile, all the above ions are structure-makers with the exceptions of the weak structure-breaking ion  $\text{ClO}_4^-$  in formamide and the border line cases of  $\text{ClO}_4^-$  in methanol and  $\text{I}^-$  in formamide.

thermodynamics of viscous flow:

Assuming viscous flow as a rate process, the viscosity  $\eta$  can be represented as using Syring<sup>97</sup> approach

$$\eta = A e^{E_{vis}/RT} = \left(\frac{hN}{V}\right) \exp \Delta G^*/RT = \left(\frac{hN}{V}\right) \exp\left(\frac{\Delta H^*}{RT} - \frac{\Delta S^*}{R}\right) \dots (34)$$

where  $E_{vis}$  is the experimental entropy of activation which is determined from a plot of  $\ln \eta$  against  $\frac{1}{T}$ .  $\Delta G^*$ ,  $\Delta H^*$  and  $\Delta S^*$  are the free energy, enthalpy and entropy of activation respectively.

The problem is dealt in a different way by Nightingale and Denck<sup>98</sup> who calculated the thermodynamics of viscous flow of salts and ions in aqueous solution.  $E_{vis}$  value can be determined using the Jones-Dole equation neglecting the  $\Delta G^*$  term. Thus,

$$R \frac{d \ln \eta}{d(1/T)} = R \frac{d \ln \eta_0}{d(1/T)} + \frac{R}{1+Bc} \frac{d(1+Bc)}{d(1/T)} \dots (35)$$

$$\Delta E_{\eta}^{\neq} = \Delta E_{\eta_0}^{\neq} + \Delta E_{\eta_{(solv)}}^{\neq} \dots (36)$$

$\Delta E_{\eta}^{\neq}$  can be interpreted as the increase or decrease of the activation energies for viscous flow for the pure solvents due to the presence of ions i.e. effective influence of the ions upon the viscous flow of the solvent molecules. The

activation energy for viscous flow in a pure liquid can be interpreted as the energy required to occupy the volume into which the molecule jumps plus that required to break the bond with other molecules if the liquid is associated. Since the number of ions are generally very very small compared to the number of the solvent molecules, the contribution of the ions to the viscous flow of solvent molecules would be generally small.

Weekins et al<sup>99</sup> have suggested an alternative formulation based on the transition treatment of the relative viscosity of the electrolytic solution. They suggested the following expression

$$\eta = \frac{(\bar{V}_1^0 - \bar{V}_2^0)}{1000} + \frac{\bar{V}_1^0}{1000} \left( \frac{\Delta \mu_2^{0\ddagger} - \Delta \mu_1^{0\ddagger}}{RT} \right) \quad \dots (37)$$

where  $\bar{V}_1^0$  and  $\bar{V}_2^0$  are the partial molal volumes of the solvent and solute respectively;  $\Delta \mu_1^{0\ddagger}$  is the free energy of activation for viscous flow per mole of the solvent which is equal to

$$\Delta \mu_1^{0\ddagger} = \Delta G_1^{0\ddagger} = RT \ln \left( \frac{n_1 V_1}{h N} \right) \quad \dots (38)$$

The quantity  $(\Delta \mu_2^{0\ddagger} - \Delta \mu_1^{0\ddagger})$  is the change in the activation energy per mole of the solute on replacing one mole of solvent by one mole of solute in an infinitely dilute solution.  $\Delta \mu_2^{0\ddagger}$  is the ionic activation energy at infinite dilution.  $\Delta \mu_2^{0\ddagger}$  has the same qualitative significance as that of  $\Delta E_V^{0\ddagger}$  but quantitatively different.

If  $\Delta H$  is known at various temperature we can calculate the ionic activation entropy and the ionic activation enthalpy.

$$d(\Delta H_2^{\circ\ddagger})/dT = -\Delta S_2^{\circ\ddagger} \quad \dots (39)$$

$$\Delta H_2^{\circ\ddagger} = \Delta H_2^{\circ\ddagger} + T\Delta S_2^{\circ\ddagger} \quad \dots (40)$$

The separation of the thermodynamic values are based on equality effects for the  $K^+$  and  $Cl^-$  ions or  $BPh_3$  and  $(1-P_e)_3BuN^+$  ions. In aqueous solution, both  $T\Delta S_2^{\circ\ddagger}$  and  $\Delta H_2^{\circ\ddagger}$  are positive for  $Li^+$  i.e. the formation of the transition state is associated with bond-breaking and a decrease in order whereas for  $Cs^+$ ,  $\Delta H_2^{\circ\ddagger}$  and  $T\Delta S_2^{\circ\ddagger}$  are negative i.e. the transition is associated with bond-making and increase in order.

#### Effects of shape and size :

This aspect of the problem has been dealt extensively by Stokes and Mills<sup>15</sup>. The ions in solution can be regarded to be rigid spheres suspended in continuum. The hydrodynamic treatment presented by Einstein<sup>78</sup> leads to the equation

$$\eta/\eta_0 = 1 + 2.5\phi \quad \dots (41)$$

in case of small volume fractions of spherical particles where  $\phi$  is the volume fraction occupied by the particles.

Modifications of the equation have been proposed by (i) Sinha<sup>100</sup> on the basis of departures from spherical shape and (ii) Vond<sup>36</sup> on the basis of the dependence of the flow patterns around the neighbouring particles at higher concentrations. However, considering the different aspects of the problem, spherical shapes have been assumed for electrolytes having hydrated ions of large effective size (particularly polyvalent monatomic cations). Thus, we have from (1)

$$2.5\phi = A\sqrt{C} + BC \quad \dots (42)$$

since  $A\sqrt{C}$  term can be neglected in comparison with  $BC$  and  $\phi = \bar{v}_1$  where  $\bar{v}_1$  is the partial molar volume of the ion. We get

$$2.5 \bar{v}_1 = B \quad \dots (43)$$

In the ideal case, the B-coefficient is a linear function of the solute partial molar volume ( $\bar{v}_1$ ) with slope equal to 2.5.

The  $B_2$  can be equated to

$$B_2 = 2.5 \bar{v} = 2.5 \times \frac{4}{3} \frac{\frac{R_2 N}{1000}}{} \quad \dots (44)$$

assuming that the ions behave like rigid spheres with an effective radii,  $R_2$  moving in a continuum.  $R_2$  calculated using the equation (44) should be close to crystallographic radii or corrected Stoke's radii if the ions are scarcely solvated and behave as spherical entities. But in general,  $R_2$  values of

the ions are higher than the crystallographic radii indicating appreciable solvation.

The number  $n_b$  of solvent molecules bound to the ion in the primary solvation shell can be easily calculated by comparing the Jones-Dole equation with Einstein's equation<sup>101</sup>

$$B_2 = \frac{25}{1000} (V_i + n_b V_s) \quad \dots (45)$$

where  $V_i$  is the molar volume of the bare ion,  $V_s$  the molar volume of the solvent.

The equation (45) has been used by a number of workers to study the nature of solvation and solvation number.

Thus, it is apparent that the  $B_{\text{ion}}^{\text{Einst}}$  can be easily calculated leading to the determination of structural contributions to  $B_{\text{ion}}^{\text{str}}$  as manifested in the change of solvation of ions.

#### Studies in mixed solvents:

Viscosity measurements in mixed solvents are very few. But the viscosity measurements in mixed solvents may well throw much light on the nature of the solvation and ion-solvent interactions. In fact, in cases of binary mixtures the study of  $\beta$ -coefficients of electrolytes can provide useful information as regards to the structural changes in water when the co-solvent is added. In order to do this, it is worth obtaining the ionic

values of the  $B_2$ -coefficients of the salts in mixed solvents. It would thus be possible to calculate the  $\Delta B_2$  coefficients of transfer, defined as

$$\Delta B_2 = \frac{B_2 \text{ (water + co-solvent mixtures)} - B_2 \text{ (water)}}{B_2 \text{ (water)}} \quad \dots \quad (46)$$

Viscosity measurements in mixed solvents have been carried out  
in recent years <sup>53, 61-67</sup>.

#### Conductance:

Conductance measurement is one of most accurate and widely used physical methods for investigation of electrolyte solutions <sup>102-103</sup>. The measurements can be made in a variety of solvents over wide ranges of temperature and pressure and in dilute solutions where interionic theories are not applicable. Fortunately for us accurate theories of electrolytic conductance are available to explain the results even upto a concentration limit of  $K_d$  ( $k$  = Debye-Hückel length,  $d$  = density of solution). Recent development of experimental technique provides an accuracy to the extent of 0.01% or even more. Conductance measurements together with transference number determinations provide an unequivocal method of obtaining single-ion values. The chief limitation, however, is the colligative-like nature of the information obtained.

Two types of useful information can be obtained from conductance measurements:

i) the mobility  $\mu$ , the velocity per unit field strength with which the ions move through solution.

ii) the variation of electrical mobility with concentrations.

These information together with theory enable us to calculate thermodynamic association or dissociation constants, ion-size parameters, solvent number, etc.

However, the choice and application of theoretical equations as well as equipment and experimental techniques are of great importance for precise measurements. These aspects have been described in details in a number of authoritative books and reviews.<sup>102-110</sup>

Conductance measurements give us equivalent conductances of solutions which are dependent upon solvent, temperature, pressure and the strength of the electrical field.

The solvent affects conductance due to its viscosity (resists the motion of ions), dielectric constant (controls the effective field strength and interionic potential affecting ion velocities, attraction between ions thereby the extent of ion-pairing) and its specific interactions with ions (affecting both mobility and association).

Variation of temperature or pressure changes the viscosity, dielectric constant and density of the solvent. In addition, temperature is proportional to the thermal energy of both ions

and solvent molecules and thus affects interactions among them. High pressure decreases free volume and forces the solution components closer together, thus changing interactions among them.

King<sup>111</sup> stressed the importance of the following aspects:

i) Accurate temperature control — A temperature control of 0.005°C is required for a precision of 0.01%.

Oil bath rather than water bath should be used to avoid capacitance coupling between the leads of electrodes, the solution and the bath.

ii) Exceptional purity of solute and solvents.

iii) Avoidance of polarisation errors and precision of the electrical measurements.

The important aspects such as preparation of solutions, bridges and conductance cells have been emphasised by a number of workers. The theory and design of alternating current bridges have been discussed in details by Jones and Joseph<sup>112, 113</sup>, Sheldovsky<sup>106</sup>, Evans and Matesich<sup>102</sup>, et al.

Since the conductometric method primarily depends on the mobility of ions, it can be suitably utilised to determine the dissociation constants of weak acids and association constants of electrolytes in aqueous, mixed and non-aqueous solvents. The conductometric method in conjunction with viscosity measurements give us much information regarding the ion-ion and ion-solvent interactions.

The study of conductance measurements were pursued vigorously both theoretically and experimentally during the last fifty years and a number of important theoretical equations have been derived. We shall dwell briefly on some of these aspects and our discussion will be limited to the studies in non-aqueous and mixed solvents.

The studies on the conductance of ionophores (completely dissociated in solutions) and ionogens (consisting of neutral molecules that yield ions by reacting with suitable solvents)<sup>114,115</sup> as a function of concentration gives the conductance at infinite dilution, the dissociation constants of ionogens, the association constants of ionophores and information about the structure of the solutions in the vicinity of the ion<sup>109</sup>.

The successful application of the Debye-Hückel theory<sup>116</sup> of interionic attraction was made by Onsager<sup>117</sup> in deriving the Kohlrausch's equation

$$\Lambda = \Lambda_0 - S\sqrt{c} \quad \dots (47)$$

where

$$S = \alpha\Lambda_0 + \beta \quad \dots (48)$$

$$\alpha = \frac{(Ze)^2 K}{3(2+\sqrt{2})\epsilon_r R T c^{1/2}} = 82.0460 \times 10^4 \frac{Z^3}{(\epsilon_r T)^{3/2}} / \text{mol}^{1/2} \text{cm}^{1/2} \quad \dots (49)$$

$$\text{and } \beta = \frac{z^2 e F K}{3\pi \eta c^{1/2}} = 82.487 \frac{z^3}{\eta(\epsilon_r T)^{1/2}} / \text{n}^{-1} \text{cm}^2 \text{mol}^{-3/2} \ell^{1/2} \quad \dots (50)$$

$\eta$  = viscosity in poise.

The equation took no account for the short range interactions and also shape or size of the ions in solutions. The ions were regarded as rigid charged spheres in an electrostatic and hydrodynamic continuum i.e. the solvent<sup>117</sup>. In the subsequent years, Pitts (1953)<sup>118</sup> and Fuoss and Onsager (1957)<sup>119</sup> independently worked out the solution of the problem of electrolytic conductance accounting for both long-range and short-range interactions.

However, the  $\Lambda^\circ$  values obtained for the conductance at infinite dilution using Fuoss-Onsager theory differed considerably<sup>117</sup> from that obtained using Pitt's theory and the derivation of the Fuoss-Onsager equation was questioned<sup>103, 120, 121</sup>. The observation was confirmed by Fuoss-Ising<sup>122</sup>. The original P.O. equation was modified by Fuoss and Hains<sup>122</sup> who recalculated the relaxation field, retaining the terms which had previously been neglected. The equation usually employed is of the form<sup>103</sup>

$$\Lambda = \Lambda^\circ - \frac{\alpha \Lambda^\circ c^{1/2}}{(1+Ka)(1+Ka/\sqrt{2})} - \frac{\beta c^{1/2}}{1+Ka} + G(Ka) \quad \dots (51)$$

where  $\sigma(\alpha)$  is a complicated function of the variable. The simplified form

$$\Lambda = \Lambda^{\circ} - S\sqrt{c} + E_1 \ln c + J_1 c - J_2 c^{3/2} \quad \dots (52)$$

is generally employed in the analysis of experimental results

where

$$ba = \frac{Ze^2}{\epsilon_r kT} = 16.7099 \times 10^4 \frac{\Sigma^6}{(\epsilon_r T)^3} / \text{mol}^{-1} \quad \dots (53)$$

$$K = 50.2916 \frac{\Sigma\sqrt{c}}{(\epsilon_r T)^{1/2}} / A^{\circ -1} \quad \dots (54)$$

$$E = E_1 \Lambda^{\circ} - E_2 \quad \dots (55)$$

$$E_1 = \frac{(Kab)^2}{24c} = 2.94257 \times 10^2 \frac{\Sigma^6}{(\epsilon_r T)^3} / \text{mol}^{-1} \quad \dots (56)$$

$$E_2 = \frac{Kab\beta}{16c^{1/2}} = 4.33244 \times 10^7 \frac{\Sigma^5}{(\epsilon_r T)^2 \eta} / \text{n}^{-1} \text{cm}^2 \text{mol}^{-2} \text{L} \quad \dots (57)$$

the  $J_1$  and  $J_2$  can be written as

$$J_1 = 2E_1 \Lambda^{\circ} \left[ \ln \left( \frac{Ka}{c^{1/2}} \right) + \Delta_1 \right] + 2E_2 \left[ \Delta_2 - \ln \left( \frac{Ka}{c^{1/2}} \right) \right] \quad \dots (58)$$

$$J_2 = \frac{Kab}{c^{1/2}} \left[ 4E_1 \Lambda^{\circ} \Delta_3 + 2E_2 \Delta_4 \right] - \Delta_5 \quad \dots (59)$$

The values of  $\Delta_f$  term are different for different theoretical treatment derived by Pitts<sup>123</sup>, Fuoss and Hahn<sup>124</sup> and Krafft<sup>125</sup>. We are giving the values for Fuoss and Hahn treatment

$$\Delta_1 = \frac{1}{b^3} \left[ 2b^2 + 2b - 1 \right] + 0.90735 \quad \dots (60)$$

$$\Delta_2 = \frac{22}{3b} + 0.01420 \quad \dots (61)$$

$$\Delta_3 = \frac{0.9571}{b^3} + \frac{1.1187}{b^2} + \frac{0.1523}{b} \quad \dots (62)$$

$$\Delta_4 = \frac{1}{b^3} \left[ 0.5738b^2 + 7.0572b - \frac{2}{3} \right] - 0.6461 \quad \dots (63)$$

$$\Delta_5 = \frac{\epsilon_2 \beta}{\Lambda^\circ} \left[ \frac{4}{3b} - 2.2194 \right] (-1.6527 \frac{\epsilon_2}{\Lambda^\circ}) \quad \dots (64)$$

$b$  is equal to the Bjerrum distance.

However, it has been found that all the equations are incomplete and in some cases fail to fit experimental data. Some of these results have been discussed elaborately by Fernandes - Prandi<sup>103</sup>. Further correction of the equation (62) was made by Fuoss and Accascina<sup>107</sup>. They took into consideration of the change in the viscosity of the solutions and assumed the validity of Walden's rule. The new equation becomes

$$\Lambda = \Lambda^\circ - S\bar{c} + Ec\ln c + J_1 c - J_2 c^{3/2} - B\Lambda^\circ c \quad \dots (65)$$

In most cases, however,  $J_2$  is made zero but this leads to a systematic deviation of the experimental data from the theoretical equations.

It has been observed that Zitt's equation gives better fit to the experimental data in aqueous solutions<sup>126</sup>.

#### Ton-nsociation:

The equation (65) as given above successfully represent the behaviour of completely dissociated electrolytes. The plot of  $\Lambda$  against  $C^{1/2}$  (limiting Onsager equation) are used to assign the dissociation or association of electrolytes. Thus, if  $\Lambda^\circ$  (experimental) is greater than  $\Lambda^\circ$  (theoretical) i.e. if positive deviations occur (ascribed to short-range hard-core repulsive interaction between ions), the electrolyte may be regarded as completely dissociated but if negative deviations ( $\Lambda^\circ_{\text{expt}} < \Lambda^\circ_{\text{theo}}$ ) or positive deviations from the Onsager limiting tangent ( $\alpha\Lambda^\circ + \beta$ ) occur, the electrolytes may be regarded to be associated. Here the electrostatic interactions are large so as to cause association between cations and anions. The difference in  $\Lambda^\circ$  (expt) and  $\Lambda^\circ$  (theo) would be considerable with increasing association<sup>127</sup>.

Conductance measurements helps us to determine the values of the ion-pair association constant  $K_h$  for the process



where  $K_A = \frac{1-\alpha}{\alpha^2 c Y_{\pm}^2}$  (67)

and  $\alpha = 1 - \alpha^2 c K_A Y_{\pm}^2$  (68)

For strong electrolytes, the constant  $K_A$  and  $\Lambda^0$  has been determined using Fuoss-Kraus equation <sup>128</sup> or Sheldovsky's equation <sup>129</sup>.

$$\frac{\tau(z)}{\Lambda} = \frac{1}{\Lambda^0} + \frac{K_A}{(\Lambda^0)^2} \cdot \frac{c Y_{\pm}^2 \Lambda}{\tau(z)} \quad \dots (69)$$

where  $\tau(z) = r(z)$  (Fuoss-Kraus) and

$1/\tau(z) = s(z)$  (Sheldovsky)

$$r(z) = 1 - z (1 - z (1 - z^{-1/2}))^{1/2} \quad \dots (69_a)$$

and  $\frac{1}{\tau(z)} \equiv s(z) = 1 + z + z^2/2 + z^3/8 + \dots$  (69\_b)

The plot of  $r(z)/\Lambda$  against  $c Y_{\pm}^2 \Lambda / \tau(z)$  should be a straight line having  $1/\Lambda^0$  for its intercept and  $K_A / (\Lambda^0)^2$  for its slope. When  $K_A$  is large, there will be considerable uncertainty in the determined values of  $\Lambda^0$  and  $K_A$  from (69). The Fuoss-Kraus conductance equation for associated electrolytes is given by

$$\Lambda = \Lambda^0 - S\sqrt{cc} + E(\alpha c) \ln(\alpha c) + J_1(\alpha c) - J_2(\alpha c)^{3/2} K_A \Lambda Y_{\pm}^2(\alpha c) \quad \dots (70)$$

The equation was modified by Justice<sup>130</sup>. The conductance of symmetrical electrolytes in dilute solutions can be represented by the equations

$$\Lambda = \alpha(\Lambda^0 - S\sqrt{c} + E(\alpha c) \ln(\alpha c) + J_1(R)\alpha c - J_2(R)(\alpha c)^{3/2}) \quad \dots (71)$$

$$(1-\alpha)/\alpha^2 c \gamma_{\pm}^2 = K_A \quad \dots (72)$$

$$\ln \gamma_{\pm} = -K_q^{1/2}/(1+K_R \sqrt{\alpha c}) \quad \dots (73)$$

The conductance parameters are obtained from a least square treatment after setting

$$R = q = \frac{e^2}{2\varepsilon KT} \quad \dots (74)$$

(Sjerrum's critical distance).

According to Justice, the method of fixing the  $\alpha$ -coefficient by setting  $R = q$  clearly permits a better-defined value of  $K_A$  to be obtained. Since the equation (71) is a series expansion truncated at the  $c^{3/2}$  term, it would be preferable that the resulting errors be absorbed as much as possible by  $J_2$  rather than by  $K_A$ , whose theoretical interest is greater as it contains the information concerning short-range cation-anion interaction.

From the experimental values of the association constant  $K_A$ , one can use two methods in order to determine the distance of closest approach  $a^{\circ}$  of two free ions to form one ion-pair. The following equation has been proposed by Fuoss<sup>131</sup>.

$$K_A = (4\pi N a^3 / 3000) \exp(e^2 / a \epsilon kT) \quad \dots (75)$$

In some cases, the magnitude of  $K_A$  was too small to permit a calculation of  $a^{\circ}$ . The distance parameter was finally determined from the more general equation due to Bjerrum<sup>132</sup>.

$$K_A = (4\pi N / 1000) \int_0^{r=9} r^2 \exp(Z^2 e^2 / r \epsilon kT) dr \quad \dots (76)$$

The equation neglects specific short-range interactions except for solvation in which the solvated ion can be approximated by a hard-sphere model. The method has been successfully utilised by Douheret<sup>133</sup>.

#### Ion-size parameter and ionic association:

The equation (63) can be written as

$$\Lambda' = \Lambda + S\sqrt{c} - E_c \log c = \Lambda^{\circ} + (J - B\Lambda^{\circ})c = \Lambda^{\circ} + J'c \quad \dots (82)$$

with  $J_2$  term omitted.

Thus, a plot of  $\Lambda'$  vs  $c$  gives a straight line with  $\Lambda^{\circ}$  as intercept and  $J'$  or  $(J - B\Lambda^{\circ})$  as slope. Assuming  $B\Lambda^{\circ}$  to be

negligible,  $a^\circ$  values can be calculated from  $J^*$ . The  $a^\circ$  values obtained by this method in 1950 were much smaller<sup>127</sup> than would be expected from sum of crystallographic radii. One of the reasons attributed to it is ion-solvent interactions which are not included in the continuum theory on which the conductance equations are based. The inclusion of dielectric saturation results in an increase in  $a^\circ$  values (such in conformity with the crystallographic radii) of alkali metal salts (having ions of high surface charge density) in sulpholane. The viscosity correction (which should be  $B \Delta C$  rather than  $B \Delta^2 C$ ) leads to<sup>133</sup> a larger values of  $a^\circ$ , still the agreement is poor. However, little of real physical significance may be attached to the distance of closest approach derived from  $J^{139}$ . For slightly associated salt, the slope of the Fuoss-Meissner equation, after correcting for viscosity, becomes  $J = K_2 Y^2 A^\circ$  and Fuoss<sup>140</sup> has shown that an unattainable precision of  $\pm 0.001\%$  would be required to resolve the two terms. If we assume a 'reasonable' value for the ion-size parameter, we could calculate  $J$  and from the corrected slope obtain a rough value of the association constant<sup>127</sup>.

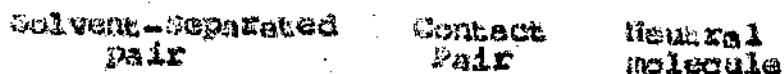
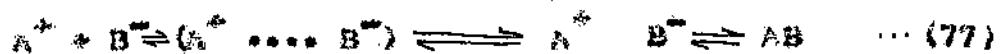
Fuoss<sup>134</sup> in 1975 proposed a new conductance equation. He<sup>134</sup> subsequently put forward another conductance equation (in 1976) which replaces the old equations suggested by Fuoss and co-workers. He classified the ions of an electrolytic solutions in one of the three categories: (1) those which find an ion of opposite charge in the first shell of nearest neighbours (contact pairs) with  $r_{ij} = a$ . The nearest neighbours

to a contact-pair are the solvent molecules which form a cage around the pairs.

(2) Those with overlapping Gurney co-spheres (solvent separated pairs). For these  $r_{ij} = (a + ns)$  where  $n$  is generally one but may be 2, 3 etc; ' $s$ ' is the diameter of a sphere corresponding to the average volume (actual plus free) per solvent molecule, contact pairs form by a sequence of ion-solvent site interchanges inside the R-spheres, until two ions of opposite charge become nearest neighbours.

(3) those which find no other unpaired ion in a surrounding sphere of radius  $R$ , where  $R$  is the diameter of the co-sphere (unpaired ions).

Thermal motion and interionic forces establish a steady state, represented by the equilibria:



Contact pairs of ionogens may rearrange to neutral molecules  $A^+ B^- \rightleftharpoons AB$  e.g.  $MgO^+$  and  $CH_3COO^-$ . Let  $\gamma$  be the fraction of solute present as unpaired ( $r > R$ ) ions. The concentration of unpaired ion is  $C\gamma$ , if  $\alpha$  be the fraction of paired ions ( $r \leq R$ ), then the concentration of the solvent-separated pair is  $C(1-\alpha)$  ( $1-\alpha$ ) and that of contact pair is  $\alpha C(1-\alpha)$ .

The equilibrium constants for (77) are

$$K_R = (1-\alpha)(1-\gamma)/c \gamma^2 f^2 \quad \dots (78a)$$

$$K_g = \alpha/(1-\alpha) = \exp(-\epsilon_g/kT) = e^{-\epsilon/kT} \quad \dots (78b)$$

where  $K_R$  describes the formation and separation of solvent-separated pairs by diffusion in and out of spheres of diameter  $a$  around cations and can be calculable by continuum theory.  $K_g$  is the constant describing the specific short-range ion-solvent and ion-ion interactions by which contact-pairs form and dissociate;  $\epsilon_g$  is the difference in energy between a pair in the states ( $r = R$ ) and ( $r = a$ ),  $\epsilon$  is measured in units K.

$$\text{Now, } 1-\alpha = 1/(1+K_g) \quad \dots (78c)$$

and the conductometric pairing constant is given by

$$K_A = (1-\gamma)/c \gamma^2 f^2 = K_R / (1-\alpha) = K_R (1+K_g) \quad \dots (79)$$

The equation determines the concentration of 'active ions' which produce long-range interionic effects. The contact pairs react as dipoles to an external field ' $\chi$ ' and contribute only to changing current. Both contact-pairs and solvent-separated pairs are left as virtual dipoles by unpaired ions, their interaction with unpaired ions is therefore neglected in calculating long-range effects (activity coefficients, relaxation field  $\Delta x$  and electrophoresis  $\Delta A_e$ ). The various patterns

can be reproduced by theoretical functions of the form

$$\Lambda = P[\Lambda^0(1+\Delta X/X) + \Delta \Lambda_e] \quad \dots (80)$$

$$= P[\Lambda^0(1+RX) + EL] \quad \dots (80a)$$

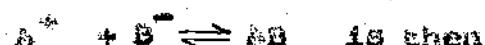
which is a three parameter equation  $\Lambda = \Lambda(C, \Lambda^0, R, E_s)$ .  $\Delta X/X$  (the relaxation field, RX) and  $\Delta \Lambda_e$  (the electrophoretic counter current, EL) are long-range effects due to electrostatic interionic forces and P is the fraction of solute which contributes to conductance current. R is the diameter of the Gurney co-sphere. The parameter  $K_g$  (or  $E_g$ ) is a catch-all for all short-range effects.

$$P = 1 - \alpha(1 - \gamma) \quad \dots (80b)$$

In case of ionogens or for ionophores in solvents of low dielectric constant,  $\alpha$  is very near to unity ( $-u_2/kT \gg 1$ ) and the equation becomes:

$$\Lambda = \gamma[\Lambda^0(1+\Delta X/X) + \Delta \Lambda_e] \quad \dots (80c)$$

The equilibrium constant for the effective reaction



$$K_A = (1 - \gamma)/C \gamma^2 \epsilon^2 \approx K_R K_B \quad \dots (80d)$$

because  $K_g \gg 1$ .

The parameters and the variables are related by the set of equations

$$\gamma = 1 - K_R \gamma^2 f^2 / (1 - \alpha) \quad \dots (81)$$

$$K_R = (4 \pi R^3 / 3000) \exp(-\epsilon / R) \quad \dots (81a)$$

$$-\ln f = \beta k / 2(1 + k_R), \beta = e^2 / D k T \quad \dots (81b)$$

$$R^2 = 8\pi\beta\gamma_n = \pi\beta N\gamma_c / 125 \quad \dots (81c)$$

$$-\epsilon = \ln [\alpha / (1 - \alpha)] \quad \dots (81d)$$

The details of the calculations are presented in the 1978 paper<sup>134</sup>. The short comings of the previous equations have been rectified in the present equation which is more general than the previous equations and can be used in the higher concentration regions (0.1 N in aqueous equations).

#### Limiting equivalent conductances

The limiting equivalent conductance of an electrolyte can be easily determined from the theoretical equations and experimental observations. At infinite dilutions, the motion of an ion is limited solely by the interactions with surrounding solvent molecules as the ions are infinitely apart. Under these conditions, the validity of Kohlrausch's law of independent migration of ions is almost axiomatic. Thus

$$\Lambda^\circ = \lambda_+^\circ + \lambda_-^\circ \quad \dots (83a)$$

At present limiting equivalent conductance is the only function which can be divided into ionic components using experimentally determined transference number of ions.

$$\text{i.e. } \lambda_+^\circ = t_+ \lambda^\circ \text{ and } \lambda_-^\circ = t_- \lambda^\circ \quad \dots \text{ (83b)}$$

thus from the accurate value of  $\lambda^\circ$  of ions, it is possible to separate the contributions due to cations and anions in the solute-solvent interactions<sup>141</sup>. However, accurate transference number determinations are limited to few solvents only. Spike<sup>142</sup> and more recently Kruyngel<sup>143</sup> have made extensive reviews on the subject.

In the absence of experimentally measured transference numbers, it would be useful to develop indirect method to obtain the limiting equivalent conductances in organic solvents for which experimental transference numbers are not yet available.

The method as have been summarized by Kruyngel<sup>143</sup> are

(i) Walden equation<sup>144</sup>

$$(\lambda_{\text{acetone}}^\pm \cdot \eta_{\text{acetone}}) = (\lambda_{\text{water}}^\pm \cdot \eta_{\text{water}}) \quad \dots \text{ (84a)}$$

$$(ii) \lambda_{\text{pic}, \text{pic}} \cdot \eta_{\text{pic}} = 0.267 \quad \dots \text{ (84b)}$$

$$\lambda_{\text{pic}, \text{pic}} \cdot \eta_{\text{pic}} = 0.296 \quad \dots \text{ (84c)}$$

Based on  $\lambda_{\text{acetone}}^\pm \cdot \eta_{\text{acetone}} = 0.563$

... (84b)

Walden considered the products to be independent of temperature and solvent. However, the  $\Lambda^{\circ}$  Et<sub>4</sub>NPF<sub>6</sub> values used by Walden was found to differ considerably from the data of subsequent more precise studies and the values of (ii) are considerably different for different solvents.

(iii)  $\lambda_0^{25}$ , Bu<sub>4</sub>N<sup>+</sup> =  $\lambda_0^{25}$ , PhHg<sup>2+</sup> (based on the equality of the  $\Lambda_0^{25}$  Bu<sub>4</sub>NBF<sub>4</sub><sup>2-</sup> and  $\Lambda_0^{25}$  Bu<sub>4</sub>NH(OEt)<sub>2</sub>Hg<sup>2+</sup> which is obviously wrong)

... (55)

(iv)  $\lambda_0^{25}$ , NaOEt<sub>2</sub>n<sup>+</sup> =  $\lambda_0^{25}$ , OctadecO<sub>4</sub><sup>2-</sup>. But this is not realized in practice <sup>147</sup>

... (56)

(v)  $\lambda_0^{25}$ , Bu<sub>4</sub>N<sup>+</sup>,  $\eta_0$       148-153  
= 0.208 ± 0.009  
= 0.206 ± 0.008  
= 0.206      ... (57)  
= 0.209  
= 0.201  
= 0.233

But from precise transfer number measurements, we obtain  $\lambda_0^{25}$ , Bu<sub>4</sub>N<sup>+</sup>,  $\eta_0$  = 0.213 ± 0.002 and the method can not be used for splitting  $\Lambda^{\circ}$ -values.

(vi)  $\lambda_0^{25}, \text{Na}_3\text{PhH}^+ = \lambda_0^{25}, \text{PhSO}_3^-$ <sup>154</sup>, the equality is observed in some solvents but not in others.

(vii)  $\lambda_0^{25}, \text{Bu}_4\text{N}^+ = \lambda_0^{25}, \text{Ph}_4\text{B}^-$ <sup>155</sup> ... (89)

The equality holds good in nitrobenzene and in mixtures with  $\text{CCl}_4$  but not realised in methanol, acetonitrile and nitromethane.

(viii)  $\lambda_0, \text{Ph}_4\text{As}^+ = \lambda_0, \text{Ph}_4\text{B}^-$ <sup>156</sup> ... (90)

may be applicable for the equal division of  $\Delta\sigma_{xy}^0$  ( $\text{Ph}_4\text{AsPh}_4$ ) but the method is not applicable to obtain limiting equivalent conductances.

(ix)  $\lambda_0^{25}, \text{Bu}_4\text{N}^+ = \lambda_0^{25}, \text{Bu}_4\text{B}^-$ <sup>157</sup> ... (91)

The method appears to be sound as the negative charge on boron in the  $\text{Bu}_4\text{B}^-$  ion is completely shielded by four inert butyl groups as in the  $\text{Bu}_4\text{N}^+$  ion while this phenomenon was not observed in case of  $\text{Ph}_4\text{B}^-$ . But the method could not be checked due to lack of accurate transference data.

(x) The equation suggested by Cill

$$\lambda_0^{25}, \text{R}_4\text{N}^+ = zp^2/6\pi n\eta [x_1 - (0.010x_0 + x_y)]$$

... (92)

$z$  and  $r_1$  = charge and crystallographic radius of proper ion;  
 $\eta_s$  and  $\epsilon_0$  = solvent viscosity and dielectric constant of the  
medium;  $r_y$  = adjustable parameter taken equal to  $0.86\text{\AA}^0$  and  
 $1.13\text{\AA}^0$  for dipolar non-associated solvents and for hydrogen-  
bonded and ether associated solvents.

However, large discrepancies were observed between the experimental and calculated values<sup>143(a)</sup>. In a recent paper<sup>143(b)</sup> Kruymal examined the Bill's approach more critically using conductance in as many all solvents and found the method reliable in three solvents e.g. butan-1-ol, acetonitrile and nitromethane.

$$(xi) \lambda_0^{25}, i\text{-Am}_3\text{Bu}_2\text{N}^+ = \lambda_0^{25}, \text{Ph}_3\text{B}^- 159 \quad \dots (93)$$

It has been found from transference measurements that the  $\lambda_0^{25}, i\text{-Am}_3\text{Bu}_2\text{N}^+$  and  $\lambda_0^{25}, \text{Ph}_3\text{B}^-$  values differ from one another only by 1%.

$$(xii) \lambda_0^{25}, i\text{-Am}_3\text{N}^+ = \lambda_0^{25}, i\text{-Am}_4^{\text{B}} \quad \dots (94)$$

The equality is not proved.

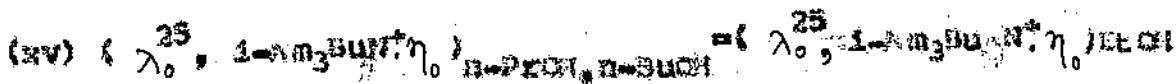
$$(xiii) \lambda_0^{25}, \text{Bu}_3\text{N}^+ = 1.08 \lambda_0^{25}, i\text{-Am}_4^{\text{N}^+} \quad \dots (95)$$

The value differs from solvent to solvent.

$$(xiv) \lambda_0^{25}, \text{Ph}_3\text{B}^- = 1.01 \lambda_0^{25}, i\text{-Am}_3^{\text{B}^-} \quad \dots (96)$$

The value is found to be true for various organic solvents.

161



161 ... (97)



... (98)

The methods (xi), (xiv) and (xv) are regarded to be the methods which can give correct single ion values for any organic solvent.<sup>143</sup>

Kruyaya<sup>143</sup> suggested a method for determining the limiting ion conductances in organic solvents or organic mixtures. The method is based on the fact that large tetraalkyl(aryl)onium ions are not solvated in organic solvents in the kinetic sense (i.e. the mobility or concentration of solvent molecules around the ions is equal to the corresponding values in the body of the solvent, which are perturbed by the influence of foreign particles) due to impossibility of the formation of donor-acceptor complexes of the ions with the solvent molecules and the extremely weak electrostatic interactions between solvent molecules and the large ions with low surface charge density. The phenomenon of non-solvation is confirmed by R.M.R. measurements and is utilised as a suitable model for apportioning  $\Lambda^\circ$  values into ionic components for non-aqueous electrolytic solutions.

Considering the motion of a solvated ion in an electrostatic field as a whole, it is possible to calculate the radius of the moving particle by the Stokes equation

$$r_s = \frac{|z|F^2}{4\pi\eta_0\lambda_0^2} \quad \dots (99)$$

where  $\lambda_0$  is a co-efficient varying from 6 (in the case of perfect sticking) to 4 (in the case of perfect slipping). Since the  $r_s$  values, the real dimension of the non-solvated tetraalkylarylium ions must be constant, we have

$$\lambda_0^2 \eta_0 = \text{Constant} \quad \dots (100)$$

This relation has been verified using  $\lambda_0^2$  values determined with precise transference numbers. The product becomes constant and independent of the chemical nature of the organic solvents for the  $\text{t-Ag}_3^+$ ,  $\text{Ph}_4\text{As}^+$  and  $\text{Ph}_4\text{S}^+$  ions and for tetraalkylammonium cations starting with  $n\text{-Et}_3\text{N}^+$ . The relationship can be well utilised to determine  $\lambda_0^2$  of ions in other organic solvents from the determined  $\Lambda^\circ$  values.

Solvation number 141

If the limiting conductance of the ion  $i$  of charge  $z_i$  is known, the effective radius of the solvated ion can easily be determined from the Stokes law. The volume of the solvation

shell  $V_s$  can be written as

$$V_s = \frac{4\pi}{3} (r_s^3 - r_c^3) \quad \dots (101)$$

where  $r_c$  is the crystal radius of the ion  $n_g$  would then be obtained from

$$n_g = \frac{V_s}{V_0} \quad \dots (102)$$

assuming Stokes' relation to hold, the ionic solvated volume should be obtained, because of packing effects<sup>162</sup> from

$$V_s^0 = 4.35 \cdot r_s^3 \quad \dots (103)$$

where  $V_s^0$  is expressed in mol/litre and  $r_s$  in angstroms.

However, the method of determination of solvation number is not applicable to ions of medium size through a number of empirical<sup>22,27,108</sup> and theoretical corrections<sup>163-166</sup> have been suggested to make the general method.

#### Stokes' law and Walden's rule

The limiting conductance  $\lambda_i^0$  of a spherical ion of radius  $R_i$  moving in a solvent of dielectric continuum can be written, according to Stokes' hydrodynamics, as

$$\lambda_i = \frac{|z_i|e|\tilde{\epsilon}|F}{6\pi\eta_0 R_i} = \frac{0.819|z_i|}{\eta_0 R_i} \quad \dots (104)$$

where  $\eta$  = macroscopic viscosity by the solvent in poise,  $R_1$  in angstroms. If the radius  $R$  is assumed to be the same in every organic solvent, as would be the case of bulky organic ions, we get

$$\lambda^0 \eta_0 = \frac{0.819 |z| I^2}{R_1} = \text{Constant} \quad \dots (103)$$

This is known as Walden's rule<sup>167</sup>. The effective radii obtained using the equation can be used to obtain solvation number. The failure of the Stokes' radii to give the effective size of the solvated ions for small ions is generally ascribed to the inapplicability of Stokes' law to molecular motions.

Robinson and Stokes<sup>108</sup>, Nightingale<sup>77</sup> and others plotted  $r_{\text{eff}}/r_s$  versus  $r_s$ ,  $r_{\text{eff}}$  versus  $r_s$  and  $r_x$  versus  $r_s$  where  $r_s$  is Stokes' radius,  $r_{\text{eff}}$  = effective radius of ion in solution which is equal to the crystal radius  $r_x$  of the large and unclaved tetrahydronium ion and obtained by calibration curves for each solvent for correcting the Stokes' radii of ions. However, the experimental results indicate that the method is incorrect as the method is based on the wrong assumption of the invariance of Walden's product with temperature.

The idea of microscopic viscosity<sup>171</sup> was invoked without much success<sup>172, 173</sup> but it has been found that

$$\lambda^0 \eta^P = \text{Constant} \quad \dots (103a)$$

where  $P$  is usually 0.7 for alkali metal or halide ions and  $P = 1$  for the large ions.<sup>174, 175</sup>

Attempts to explain the change in the Stokes' radius  $R_i$  have been made. The apparent increase in the real radius  $r$  has been attributed to ion-dipole polarisation and the effect of dielectric saturation on  $R$ . The dependence of the Walden product  $\lambda^0 \eta_0$  on the dielectric constant led Fuoss to consider the effect of the electrostatic forces on the hydrodynamic of the system, considering the excess frictional resistance caused by the dielectric relaxation in the solvent caused by ionic motion. Fuoss proposed the relation

$$\lambda_{i,0}^0 = \frac{\bar{F}_e |Z|}{6\pi R_\infty (1 + A/\epsilon R_\infty^2)} \quad \dots (106)$$

$$\text{or} \quad R_i = R_\infty + A/\epsilon \quad \dots (107)$$

where  $R_\infty$  is the hydrodynamic radius of the ion in an hypothetical medium of dielectric constant where all electrostatic forces vanish.

Boyd<sup>184</sup> gave the expression

$$\lambda_i^0 = \frac{\bar{F}_e |Z|}{6\pi \eta_0 r_i} \left[ 1 + \frac{2}{27} \frac{1}{\pi \eta_0} \frac{Z^2 e^2 \tau}{r_i^4 \epsilon_0} \right] \quad \dots (108)$$

considering the effect of dielectric relaxation on ionic motion;  $\tau$  is the Debye relaxation time for the solvent molecules.

<sup>165</sup> Swanson treated the ion as a rigid sphere of radius  $r_i$  moving with a steady state velocity  $v_i$  through a viscous incompressible dielectric continuum. The conductance equation suggested by Swanson is

$$\lambda_i^o = \frac{Z_i e F}{A_0 \pi r_i \eta_i + A_D [Z_i^2 e^2 (\epsilon_r^o - \epsilon_r^\infty) \tau / \epsilon_r^o (2\epsilon_r^o + 1) r_i^3]} \quad \dots (109)$$

$\epsilon_r^o$ ,  $\epsilon_r^\infty$  are the static and the limiting high-frequency (optical) dielectric constants,  $A_V = 6$  and  $A_D = \frac{3}{8}$  for perfect sticking and  $A_V = 4$  and  $A_D = \frac{3}{4}$  for perfect slipping.

$$\lambda_i^o = A r_i^3 / (r_i^4 + B) \quad \dots (110)$$

The theory predicts <sup>177</sup> that  $\lambda_i^o$  passes through a maximum of  $27^{1/4} A^{1/4} B^{1/4}$  at  $r_i = (3B)^{1/4}$ . The phenomenon of maximum conductance is well known. The relationship holds good to a reasonable extent for cations in aprotic solvents but fails in case of anions. The conductance, however, falls off rather more rapidly than predicted with increasing radius.

For comparison of results in different solvents, the  
equation can be rearranged as<sup>178</sup>

$$\frac{Z_i^2 e F}{\lambda_i^0 \cdot n_0} = A_V \pi r_i + \frac{A_D Z_i^2}{r_i^3} \cdot \frac{e^2 (\epsilon_r^0 - \epsilon_r^\infty)}{\epsilon_r^0 (2\epsilon_r^0 + 1)} \cdot \frac{T}{n_0} \quad \dots (111)$$

or  $L^* = A_V \pi r_i + \frac{A_D Z_i^2}{r_i^3} P^* \quad \dots (112)$

In order to test Swanzig's theory the equation (112) was applied to methanol, ethanol, acetoneitrile, butanol and pentanol solutions where accurate conductance and transference data are available<sup>177-182, 161</sup>. All the plots were found to be straight lines. But the radii calculated from the intercepts and slopes are far apart from equal except in some cases where moderate success is noted. It is noted that the relaxation effect is not the predominant factor affecting ionic mobilities and that these mobility differences could be explained qualitatively if the microscopic properties of the solvent, dipole moment and free electron pairs were considered the predominant factors in the deviation from Stokes' law<sup>161</sup>.

It is noted that the Swanzig theory is successful for large organic cations in aprotic media where solvation is likely to be minima and where viscous friction predominates over that caused by dielectric relaxation. The theory breaks down whenever the dielectric relaxation term becomes large i.e. for

solvents for high  $\mu^*$  and for ions of small  $r_1$ . Like any continuum theory Swanson has the inherent weakness of its inability to account for the structural features<sup>183</sup> e.g.

- (1) It does not allow for any correlation in the reorientation of the solvent molecules as the ion passes by and this may be the reason why the equation do not apply to hydrogen bonded solvents<sup>184</sup>.
- (2) The theory does not distinguish between positively and negatively charged ions and therefore can not explain why certain anions in dipolar aprotic media possess considerably higher molar conductances than the fastest cations<sup>183</sup>.

The Walden product in case of mixed solvents does not show any constancy but it shows a maximum in case of DME + H<sub>2</sub>O<sup>185-187</sup> and DMA + H<sub>2</sub>O<sup>188</sup> mixtures and other aqueous binary mixtures<sup>185-188</sup>.

- To derive expressions for the variation of the Walden products with the composition of mixed polar solvents, various attempts<sup>164, 165, 189</sup> have been made with different models for ion-solvent interactions but no satisfactory expression has been derived taking into account all types of ion-solvent interactions as : (1) It is difficult to include all types of interactions between ions as well as solvents in a single mathematical expression;
- (2) it is not possible to account for some specific properties of different kinds of ions and solvent molecules<sup>185</sup>. Ions moving in a dielectric medium experience a friction force due to

dielectric loss arising from ion-solvent interactions with the hydrodynamic force. Swanson's expression though account for a change in Walden product with solvent composition but does not account for the maxima. Nemeth<sup>190</sup> suggested that the major deviations in the Walden product is due to the variation of the electrochemical equilibrium between ions and solvent molecules with the composition of mixed polar solvents. In cases where more than one type of solvated complexes are formed, there should be a maximum and/or a minimum in the Walden product. This is supported from experimental observations. Hubbard and Onsager<sup>191</sup> have developed the kinetic theory of ion-solvent interaction within the framework of continuum mechanics where the concept of kinetic polarisation deficiency has been introduced. Lal Behadur and Ramamurti<sup>135-137</sup> explained the variation of Walden product (in DMF + H<sub>2</sub>O and DMA + H<sub>2</sub>O mixtures) on the basis of hydrophobic hydration of ions due to co-solvent DMF or DMA giving excess mobility of ions producing a maximum in Walden product in the water rich region whereas solvation of ions with DMF or DMA will be more effective in the DMF or DMA rich region resulting in further decrease of Walden product.

However, quantitative expression is still awaited. Further improvements naturally must be in terms of (1) sophisticated treatment of dielectric saturation, (2) specific structural effects involving ion-solvent interactions.

2-methoxy ethanol (ME) and 1,2-dimethoxy ethane (DME)

The present thesis embodies the results based on viscometric and conductometric measurements, on ion-solvent interactions of some tetraalkylammonium halides and alkali metal halides in some non-aqueous and mixed aqueous co-solvents. The co-solvent chosen for such studies are 2-cosolvents viz. methyl cellosolve (1,2-dimethoxyethane, DME).

Chemically these solvents are mono- and dimethyl ethers of ethylene glycol (EG) --- a solvent well studied with regard to ion-solvent interactions. The study on ion-solvent interactions in these cosolvent system are likely to reflect the effect of increasing number of methyl groups (electron releasing inductive effect) and decreasing number of OH groups.

In studies<sup>190</sup> indicated that the predominant configurations of ME molecule in the gauche form to facilitate intermolecular hydrogen bonding as shown in structure Ia. Since no intramolecular hydrogen bonding is feasible in pure DME, the predominant configuration of DME is the trans of Ia.

Simple consideration of molecular structure indicates that due to the presence of electron repelling inductive effect of  $\text{CH}_3$  in methoxy group, ME is more basic than ethylene glycol and water. Also, the restricted availability of the acidic H-atom of CH group makes ME molecules less acidic than ethylene glycol and water, thus imparting a 'quasi-aprotic' character

to it. On the other hand, due to the inductive effect of two  $\text{CH}_3$  groups, the two O-centres of DMF molecules are more basic as compared to that of Water, EG and ME. But due to the absence of any acidic hydrogen atom DMF is a typically aprotic solvent.

Moreover, the basicity and proticity are likely to be relayed through co-operative structure of H-bonding<sup>199</sup> between the co-solvent and water molecules in aqueous solutions. Thus in ME +  $\text{H}_2\text{O}$  system, the possible H-bonded co-solvent Water complex of the type IIIA is also more basic and less acidic than Water and EG-water mixtures. In DMF-water system the possible H-bonded aquo-DMF complexes are of the type IIIB and IIIC, in equilibrium with each other, the former predominant at water rich composition, the later at water deficient compositions. It is to be noted that since a gauche form around  $-\text{CH}_2-\text{CH}_2-$  group is likely to be more favourable for association, it may influence the equilibrium between trans and gauche forms in favour of gauche form as shown in IIIC. In aqueous solutions of DMF both IIIB and IIIC are more basic and less acidic than water, hence the mixed solvents as a whole are likely to be increasingly more basic and at the same time less acidic than not only to water but also to ME. Thus the order of basicity to be : water < ME < DMF. Also the relative acidities would increased in the reverse order.

Studies on fundamental physico-chemical properties like density<sup>200</sup>, dielectric constants<sup>201</sup> for ME water mixtures have

been reported at different temperatures throughout the composition range. Both properties are found to decrease monotonically with composition. For DME-water system also these values at different temperatures are available<sup>198</sup>. Desnoyers and co-workers<sup>201</sup> have reported apparent molar volume and heat capacities of aqueous ME at water rich compositions at 25°C and showed that ME behaves as a fairly typical polar non electrolyte in water. Heat capacity and heat of solution of ME<sup>202</sup> and DME<sup>202</sup> have been reported by number of workers. Partial molar volume<sup>203</sup> of DME and ME have been studied with water. The change in free energy, entropy and enthalpy associated with transfer of ME and DME from ideal gas phase to dilute aqueous solution at 25°C have also been reported.

Notably enough, relatively few studies have been reported with aqueous 2-methoxy ethanol, and 1,2-dimethoxy ethane as solvent media. Renard and Justice<sup>205</sup> studied the conductometric behaviour of CsCl in DME-water mixtures as compared to dioxane-water and THF-water mixtures and the different observed for the ion-association were interpreted in terms of difference in aprotic nature of the organic molecule and that of H<sub>2</sub>O. Solvent effect of DME, on sodium salt ion-pairs, as compared to THF and other solvents were studied<sup>206</sup> from NMR spectra. Conductance behaviour of ion-pair formation of tetrabutyl-ammonium bromide in aquo-ME<sup>207</sup> at 25°C was interpreted on the basis of modification water structure, depending on the nature

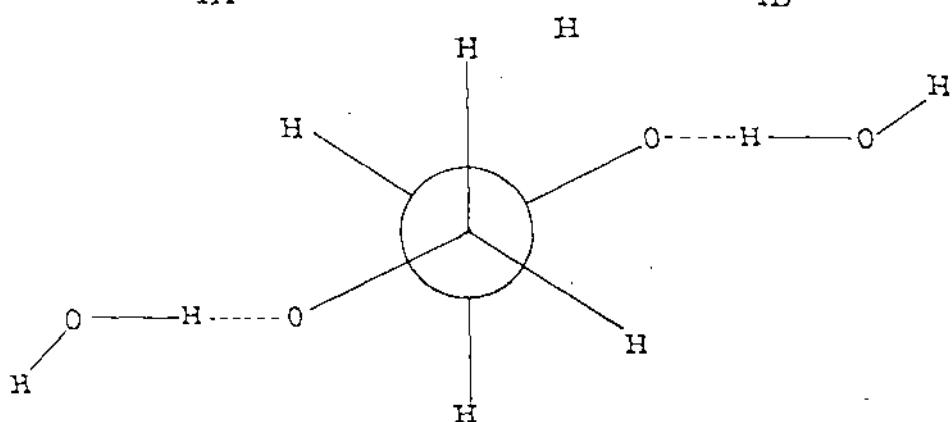
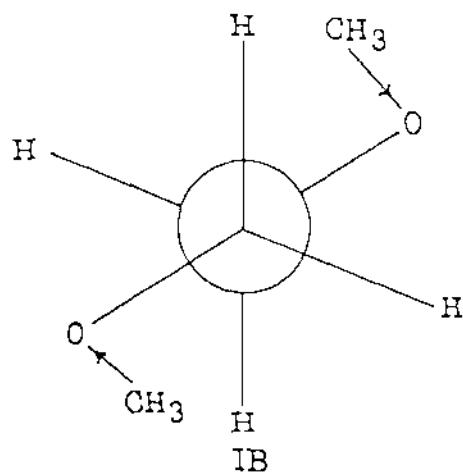
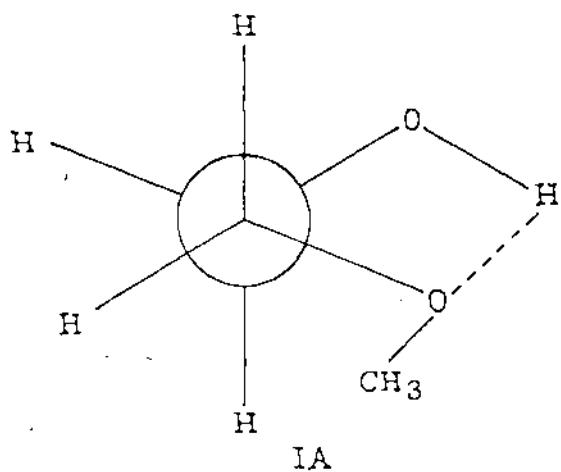
of the solvent. Salta<sup>208</sup> studied the relation between the structure of water mixtures of organic solvents, their solvation and cation exchange selectivity of metal ions in aqueous-MG.

Moroi and co-workers<sup>209</sup> also predicted the relation between free energy of transfer and selectivity of an ion exchanger. Activity coefficients of NaCl in water mixtures of MG and DMS at 25°C were studied by Richard et al.<sup>210</sup>.

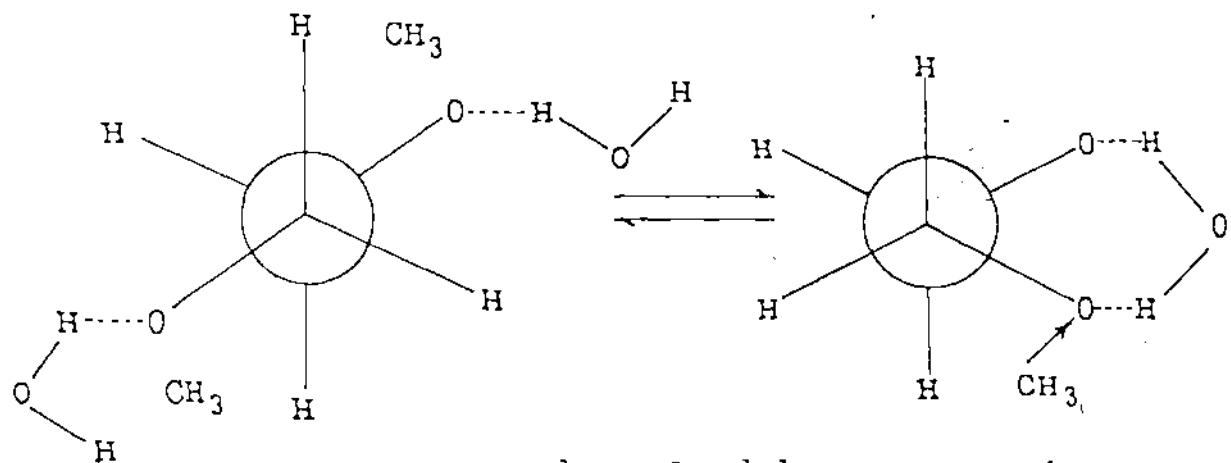
Works involving pure MG and DMS are comparatively large in number. Of these studies on dielectric properties at various temperature ( $\sim 20^{\circ}\text{C}$  to  $50^{\circ}\text{C}$ )<sup>211</sup> of MG and DMS<sup>212</sup>, solubility studies on alkali metal chlorides, temperature dependence of electrolytic conductance of salts in MG<sup>213</sup>, calculation of ionic solvation, free energies and entropies of transfer of gaseous univalent ions using continuum model in DMS<sup>214</sup>, dissociation constant studies of pure MG<sup>215</sup> and various thermodynamic studies, density, dielectric properties, viscosity etc. are noteworthy. Studies on the rate of formation and stability of some organometallic complexes<sup>216</sup> in DMS are also very much useful as they provide sufficient evidence for the existence of specific cation solvating effect of the solvent and such studies first led to the prediction of tetra-coordinated DMS-alternate metal ion complexes<sup>216</sup>, a view still considered as valid and is very much useful in studies of ion-solvation of MG.

again NB and DME are commercially known as 'Cellulosolves' being used extensively as a solvating agents for cellulose. ME finds its use in various chemical reactions, and in analytical practice<sup>217</sup>, in acid-base conductometric titrations<sup>218</sup>, electrolytes for high voltage capacitors and anti-icing additive for air-craft fuels. DME is used, now-a-days extensively as an electrochemical solvent in non-aqueous battery electrolyte, and also as solvents for the preparation and reaction of organo-alkali and organo-alkaline earth compounds<sup>215</sup>. Consequently, the knowledge of ion-solvent interactions of different solutes in these solvents are, therefore, capable of indicating the potential usefulness in various technologies, e.g. high energy non-aqueous batteries, ion exchangers etc. Transport parameters of electrolytic solutions such as ionic conductance and viscosity can provide information concerning the nature of the kinetic entities from which the ion-solvent interaction can be inferred.

We have, therefore, devoted our attention to the study of the transport properties in ME, DME and their aqueous binary mixtures.



IIA Hydrogen bonded ME-H<sub>2</sub>O complex



## B E E E A S N G E S

1. R.G. Bates, J. Electroanal. Chem., 29, 1, 1972.
2. G.S. Kell, C.M. Davies and J. Gorynski in water and aqueous solutions, structure, thermodynamics and transport process, Ed. R.A. Homs, Wiley-Interscience, 1972, Chapters 9 and 10.
3. J.G. Muischnek-Gould and K.J. Iaidler in Chemical Physics of Ionic Solutions, Ed. B.B. Conway and R.G. Barradas, John Wiley and Sons Inc. New York, 1966, p 73-86.
4. Solute-Solvent Interactions, Ed. J.R. Costanzo and C.D. Ritchie, Marcel Dekker, New York, 1969.
5. The Chemistry of Non-aqueous Solvents, Ed. J.J. Lagowski, Academic Press, New York, 1966.
6. E.S. Ans and J.P. Hinton, Solvent effects on Chemical Phenomena, Academic Press, New York, 1973.
7. The Organic Chemistry of electrolyte solutions, Ed. J.E. Gordon, Wiley-Interscience, 1975.
8. H.S. Harned and B.B. Owen, The Physical Chemistry of Electrolytic Solutions, Reinhold Publishing Corporation, New York, Third Ed., 1958.
9. Chemical Physics of Ionic Solutions, Ed. B.B. Conway and R.G. Barradas, Wiley, New York, 1966.

10. Physical Chemistry of Organic Solvent Systems, Ed. A.K. Covington and J. Dickinson, Plenum Press, London and New York, 1973.
11. F. Franks, in Water - A comprehensive treatise, Ed. F. Franks, Vol. 1, Plenum, 1973.
12. F. Franks, in Physico-Chemical Process in Mixed aqueous Solvents, Ed. F. Franks, Heinemann Educational Books Ltd. 1967, p 141-157.
13. a) V. Gutmann, Electrochim Acta, 21, 661, 1976.  
b) U. Meyer and V. Gutmann, Adv. Inorg. Chem. Radiat. Chem., 17, 169, 1975.
14. R.G. Pearson, "Hard and Soft Acids and Bases" Dowden, Hutchinson and Ross, Stroudsburgh, 1973.
15. R.H. Stokes and R. Mills, Viscosity of Electrolytes and related properties, Pergamon Press Ltd., 1965.
16. Y. Vassilow in Water and aqueous solutions, Ed. R.A. Horne, Wiley-Interscience, 1972, Chapter 12.
17. Grüneisen, Wien, Abhandl. Physik-techn. Reich-anstalt, 4, 239, 1903.
18. G. Jones and M. Cole, J. Am. Chem. Soc., 51, 2950, 1929.
19. P. Debye and E. Hückel, Physik Z., 24, 185, 1923.

20. H. Falkenhagen and H. Boie, *Z. Phys.*, **30**, 611, 1929.
21. H. Falkenhagen, *Z. Phys.*, **32**, 745, 1931.
22. H. Falkenhagen and E.L. Vernon, *Phil. Mag.*, **24**, 537, 1932.
23. L. Onsager and R.H. Fuoss, *J. Phys. Chem.*, **36**, 2689, 1932.
24. Ref. 8, p 240.
25. H. Katincky, *Z. Phys. Chem. (Frankfurt)*, **12**, 206, 1957.
26. G. Desnoyers and G. Perron, *J. Colloid. Chem.*, **1**, 199, 1972.
27. R.J.M. Bicknell, K.G. Lawrence and D. Peakins, *J. Chem. Soc. Faraday I*, **76**, 637, 1980.
28. H.P. Yeo and H.N. Bonnion, *J. Phys. Chem.*, **75**, 1727, 1971.
29. R.B. Ray, T. Vituccio, G. Sawoyski and D.F. Evans,  
*J. phys. Chem.*, **70**, 2335, 1966.
30. H. Katincky, *Diss. Faraday Soc.*, **24**, 171, 1957.
31. D. Peakins and K.G. Lawrence, *J. Chem. Soc.*, **A**, 212,  
1966.
32. Andrade, *Phil. Mag.*, **17**, 698, 1934.
33. D.E. Goldsack and R.C. Franchetto, *Can. J. Chem.*, **55**,  
1062, 1977.
34. D.E. Goldsack and R.C. Franchetto, *Can. J. Chem.*, **56**,  
1442, 1978.
35. D. Bagland and C. Pilling, *J. Phys. Chem.*, **76**, 1902, 1972.
36. J. Venz, *J. Phys. Chem.*, **52**, 277, 1948.
37. S.P. Mouluk, *J. Indian Chem. Soc.*, **49**, 483, 1972.
38. D.G. Thomas, *J. Colloid Sci.*, **20**, 267, 1965.

39. C.A. Angell, *J. Phys. Chem.*, **70**, 2793, 1966.
40. C.A. Angell, *J. Chem. Phys.*, **46**, 4673, 1967.
41. K. Roy Chowdhury and D.K. Majundar, *Electrochim. Acta*, **28**, 23, 1983.
42. K. Roy Chowdhury and D.K. Majundar, *Electrochim. Acta*, **28**, 597, 1984.
43. K. Roy Chowdhury and D.K. Majundar, *Electrochim. Acta*, **29**, 1371, 1984.
44. P.P. Rastogi, *Bull. Chem. Soc. Japan*, **63**, 2442, 1970.
45. R. Gopal and P.P. Rastogi, *Z. Physik. Chem. (N.F.)*, **69**, 1, 1970.
46. N. Tanaka, Y. Chiba and Y. Ieomura, *Bull. Chem. Soc. Japan*, **66**, 1551, 1973.
47. C.M. Criss and M.J. Mastroianni, *J. Phys. Chem.*, **75**, 2632, 1971.
48. P.K. Mandal, B.K. Seal and A.S. Basu, *Z. Physik. Chem. (Leipzig)*, **258**, 809, 1977.
49. P.K. Mandal, B.K. Seal and A.S. Basu, *Z. Physik. Chem. (N.F.)*, **97**, 295, 1973.
50. P.K. Mandal, B.K. Seal and A.S. Basu, *Z. Physik. Chem. (Leipzig)*, **259**, 909, 1977.
51. B.K. Seal, B.K. Chatterjee and P.K. Mandal, *Ind. J. Chem.*, **21**, 509, 1952.

52. A. Sacco, G. Petrella and M.D. Monika, J. Chem. Soc. Faraday I, 75, 2325, 1979.
53. A. Sacco, G. Petrella, A.D. Atti and A.D. Giglio, J. Chem. Soc. Faraday I, 78, 1507, 1982.
54. P.P. Palusz and T.V. Rebagay, J. Phys. Chem., 79, 2493, 1975.
55. A. Sacco, G. Petrella and M. Castagnolo, J. Phys. Chem., 80, 749, 1976.
56. R.K. Bhakta and Y.P. Rayal, Ind. J. Chem., 15A, 36, 1977.
57. S.K. Vijayakrishna, Ind. J. Chem., 17A, 511, 1979.
58. K. Kurotaki and S. Kawamura, J. Chem. Soc. Faraday I, 77, 217, 1981.
59. A. Sacco, G. Petrella, M. Della Monica and M. Castagnolo, J. Chem. Soc. Faraday I, 73, 1936, 1977.
60. N. Martinus and C.A. Vincent, J. Chem. Soc. Faraday Trans I, 77, 141, 1981.
61. E.I. Ivanova and N.N. Davydova, Z. Fiz. Khim., 54, 1465, 1980.
62. N.C. Das and P.B. Das, Ind. J. Chem., 15A, 826, 1977.
63. B.N. Prasad, N.P. Singh and N.M. Singh, Ind. J. Chem., 14A, 322, 1976.

64. B.N. Prasad and Hira Agarwal, Ind. J. Chem. 15A, 343, 1976.
65. J.W. Nokesall, R. Martinus and G.A. Vincent, J. Chem. Soc. Faraday I, 72, 654, 1976.
66. A. Sacco, A.D. Giglio, A.B. Atti and R. Castagnolo, J. Chem. Soc. Faraday I, 79, 431, 1983.
67. J. Domenech and S. Rivero, J. Chem. Soc. Faraday I, 80, 1249, 1984.
68. R.T.M. Bicknell, K.G. Lawrence, R.A. Scelley, D. Weakins and L. Verblan, J. Chem. Soc. Faraday I, 72, 307, 1976.
69. A. Sacco, A.D. Giglio and A.B. Atti, J. Chem. Soc. Faraday I, 77, 2693, 1981.
70. D.S. Gill and A.B. Sharma, J. Chem. Soc. Faraday I, 78, 475, 1982.
71. K.G. Lawrence and A. Sacco, J. Chem. Soc. Faraday I, 79, 615, 1983.
72. a) A. Sacco, M.B. Nonica, A.B. Giglio and K.G. Lawrence, J. Chem. Soc. Faraday I, 79, 2631, 1983.  
b) K.G. Lawrence, T.W. Bicknell, A. Sacco and A. Bell'atti, J. Chem. Soc. Faraday Trans I, 81, 1133, 1985.  
c) P.T. Thomson, K. Durban, J.E. Turner and K.H. Wood, J. Polym. Chem., 9, 935, 1980.

- 6) P.T. Thomson, B. Fisher and R.H. Wood, *J. Soln. Chem.*, 11, 1, 1982.
73. J.I. Kim, *J. Phys. Chem.*, 82, 191, 1978.
74. M. Castagnolo, G. Petrella, M.D. Monica and A. Sacco, *J. Soln. Chem.*, 8, 501, 1979.
75. W. H. Cox and J.H. Wolfenden, *Proc. Roy. Soc. London*, 195A, 475, 1934.
76. R.W. Gurnay, *Ionic Processes in Solution*, McGraw Hill, 1953.
77. E.R. Nightingale, *J. Phys. Chem.*, 63, 1381, 1959.
78. A. Einstein, *Ann. Phys.*, 19, 289, 1906.
79. C.S. Benson and A.R. Gordon, *J. Chem. Phys.*, 13, 473, 1945.
80. D.P.T. Tuan and K.M. Fuoss, *J. Phys. Chem.*, 67, 1343, 1963.
81. C.H. Springer, J.F. Coetzee and R.L. Kay, *J. Phys. Chem.*, 73, 471, 1969.
82. G. Petrella and A. Sacco, *J. Chem. Soc. Faraday I*, 74, 2070, 1978.
83. B.S. Krungals, *J. Chem. Soc. Faraday I*, 76, 1273, 1980.
84. B.S. Krungals, Russ. *J. Phys. Chem.*, 46, 858, 1972; 47, 528, 1973.
85. B.S. Krungals, Russ. *J. Phys. Chem.*, 47, 956, 1973.
86. B.S. Krungals, Russ. *J. Phys. Chem.*, 49, 1163, 1973.
87. B.S. Krungals, Russ. *J. Phys. Chem.*, 49, 1448, 1971.
88. H.P.B. Jenkins and N.S.H. Pritchett, *J. Chem. Soc. Faraday I*, 80, 721, 1984.

89. K. Tajorue, Naturwissenschaften, 2, 729, 1921.
90. D.F.C. Morris, Struct. Bonding, 2, 157, 1969.
91. R.H. Gurney, Ionic Processes in Solutions, Dover, New York, 1962.
92. H.S. Frank and W.Y. Wen, Disc. Farad. Soc., 24, 133, 1957.
93. Aemus, Z. Naturforsch., 4A, 589, 1949.
94. M.H. Abraham, J. Liszi and L. Munkacsy, J. Chem. Soc. Faraday I, 78, 197, 1982.
95. M.H. Abraham, J. Liszi and L. Munkacsy, J. Chem. Phys., 70, 249, 1979.
96. M.H. Abraham and J. Liszi, J. Chem. Soc. Faraday I, 76, 1219, 1980.
97. S. Glasstone, K.J. Laidler and H. Eyring, The Theory of Rate Processes (McGraw Hill, New York, 1941, p 477).
98. R.R. Nightingale and R.P. Benck, J. Phys. Chem., 63, 1777, 1959.
99. D. Peatling, D.J. Freemantle and K.G. Lawrence, J. Chem. Soc. Faraday I, 70, 795, 1974.
100. Sinha, J. Phys. Chem., 44, 25, 1940.
101. D. Peatling and K.G. Lawrence, J. Chem. Soc. A, 212, 1966.
102. D.P. Evans, Sister Mary and L. Batesich in Electrochemistry, Vol. 2. Ed. E. Yeager and A.J. Salkind, John Wiley and Sons, Inc. 1973, Chapter 1.

103. R. Fernandes-Prini in *Physical Chemical of Organic Solvent Systems*, Ed. A.K. Covington and J. Dickinson, Plenum Press 1973, Chapter 5.
104. D.A. Mc Innes, *The Principles of Electrochemistry*, Reinhold Published Corporation, 1961.
105. S. Glasstone, *An Introduction to Electrochemistry*, Van Nostrand, New York, 1942.
106. T. Sheldovskiy in *Techniques of Organic Chemistry*, Vol. 1, Part 4 (Ed. A. Weissberger) 3rd Ed. Wiley, New York (1939) p 3011-3048.
107. R.W. Fuoss and F. Accascina, *Electrolytic Conductance*, Interscience, New York, 1959.
108. R.A. Robinson and R.H. Stokes, *Electrolyte Solutions*, 2nd Ed. Butterworths, London, 1959.
109. J. Barthel, *Angew. Chem. Interact.* Edit. 2, 260, 1968.
110. J. Barthel and C.P. Robbins, *J. Chem. Ed.*, 48, 52, 1971.
111. B.J. King, *acid-base Equilibria*, Pergamon Press, 1965.
112. G. Jones and R.C. Joseph, *J. Am. Chem. Soc.*, 50, 1049, 1928.
113. G. Jones and B.C. Bradshaw, *J. Am. Chem. Soc.*, 55, 1780, 1933.
114. G.W. Davies, *Zeta association*, Butterworths, London, 1962.
115. R.W. Fuoss, *J. Chem. Educ.* 32, 527, 1955.

116. L. Onsager, *Physik Z.*, 28, 277, 1927.
117. R.M. Fuoss, *Rev. Pure Appl. Chem.*, 15, 125, 1963.
118. E. Pitts, *Proc. Roy. Soc.*, 217A, 43, 1953.
119. R.M. Fuoss and L. Onsager, *J. Phys. Chem.*, 61, 668, 1957.
120. R.M. Fuoss, in *Chemical Physics of Ionic Solutions*, Eds. S.N. Conroy and R.G. Barradas, Wiley, New York, 1966, p. 462.
121. E. Pitts, R.B. Fabor and J. Daly, *Trans. Faraday Soc.*, 65, 849, 1969.
122. R.M. Fuoss and K.L. Heis, *Proc. Natl. Acad. Sci.*, 59, 1550, 1967; *J. Am. Chem. Soc.*, 80, 3055, 1958.
123. R. Fernandez-Prini, *Trans. Faraday Soc.*, 65, 3311, 1969.
124. R. Fernandez-Prini and J.R. Evans, *Z. Phys. Chem. (Leipzig)* 28B, 373, 1965.
125. W.B. Kruse, *Z. Phys. Chem. (Leipzig)*, 237, 289, 1968.
126. D.E. Evans and R.L. Key, *J. Phys. Chem.*, 70, 366, 1966.
127. D.E. Arrington and D. Grinewold, *J. Phys. Chem.*, 74, 123, 1970.
128. R.M. Fuoss and C.A. Kraus, *J. Am. Chem. Soc.*, 55, 476, 1933.
129. T. Shedlovsky, *J. Franklin Inst.*, 225, 739, 1938.
130. C. Atlani and J.C. Justice, *J. Soln. Chem.*, 4, 935, 1975.
131. Ref. 107, p. 207.
132. M. Ujerrum, *Dan. Vidensk. Selek.*, 1, No. 9, 1926.

133. H. Tissier and G. Bonheret, *J. Soln. Chem.*, 7, 97, 1978.
134. R.H. Fuoss, *J. Phys. Chem.*, 49, 525, 1945; 52, 2427, 1948;  
*Proc. Natl. Acad. Sci., USA* 75, 16, 1978.
135. L. Bahadur and M.V. Ramamurti, *J. Chem. Soc. Faraday* 76, 1409, 1980.
136. L. Bahadur and M.V. Ramamurti, *J. Electrochem. Soc.*, 128, 339, 1981.
137. L. Bahadur and M.V. Ramamurti, *Can. J. Chem.*, 62, 1051, 1984.
138. R. Fernandez-Prini and J. Prue, *Trans. Farad. Soc.*, 62, 1257, 1966.
139. R.H. Fuoss and L. Onsager, *J. Phys. Chem.*, 66, 1722, 1962; 67, 621, 1963.
140. R.H. Fuoss, L. Onsager and J.F. Skinner, *J. Phys. Chem.*, 69, 2581, 1965.
141. J. Sadova, in *Water and Aqueous Solutions*, Ed. by R.N. Horne, Wiley Interscience, 1972, Chapter 4.
142. M. Spiro, in *Physical Chemistry of Organic Solvent Systems*, Ed. A.K. Covington and T. Dickinson, Plenum, 1973, Chapter 5, Part 2.

143. (a) B.S. Kruyjala, J. Chem. Soc. Faraday I, 79, 571, 1983.  
(b) B.S. Kruyjala, J. Chem. Soc. Faraday I, 81, 241-243,  
1985.
144. P. Walden, H. Ulich and Z. Bush, Z. Phys. Chem., 123,  
429, 1926.
145. P. Walden and E.J. Birr, Z. Phys. Chem., 144, 269, 1929.
146. R.H. Fowler and C.A. Kraus, J. Am. Chem. Soc.,  
62, 2237, 1940.
147. W.B. Thompson and C.A. Kraus, J. Am. Chem. Soc.,  
69, 1016, 1947.
148. H.L. Pickering and C.A. Kraus, J. Am. Chem. Soc., 71,  
3288, 1949.
149. R.H. Smiley and A.H. Martell, J. Am. Chem. Soc., 73,  
3296, 1951.
150. F. Accassina, S.L. Swarts, P.L. Mercier and C.A. Kraus,  
Proc. Natl. Acad. Sci., U.S.A. 39, 917, 1953.
151. G.R. Lester, T.A. Cover and P.G. Sears, J. Phys. Chem.,  
60, 1076, 1956.
152. H.H. Smiley and P.G. Sears, Trans. Kentucky Acad. Sci.,  
18, 40, 1957.
153. U. Mayer, V. Gutmann and L. Jodzinska, Monatsch. Chem.,  
104, 1045, 1973.

154. L.R. Dawson, E.D. Wilhoit, R.R. Holmes and P.G. Sears,  
J. Am. Chem. Soc., 79, 3004, 1957.
155. R.M. Fuoss and R. Hirsch, J. Am. Chem. Soc., 82,  
2013, 1960.
156. K. Bose and K.K. Kundu, Ind. J. Chem., 17A, 122, 1979.
157. S. Takezawa, Y. Kondo and N. Tokura, J. Phys. Chem.,  
77, 2133, 1973.
158. (a) D.S. Gill, J. Chem. Soc. Faraday I, 77, 751, 1981.  
(b) D.S. Gill, U. Kumari and H.S. Chauhan, J. Chem. Soc.  
Faraday Trans I, 81, 687, 1985.
159. W.A. Coplen and R.M. Fuoss, J. Phys. Chem., 68, 1177, 1964.
160. J.F. Coetzee and G.P. Cunningham, J. Am. Chem. Soc.,  
87, 2629, 1965.
161. D.F. Evans and P. Gardam, J. Phys. Chem., 72, 3281, 1968;  
73, 158, 1969.
162. R.H. Stokes and R.A. Robinson, Trans. Farad. Soc.,  
53, 301, 1957.
163. H. Born, Z. Physik, 1, 221, 1920.
164. R.H. Boyd, J. Chem. Phys., 35, 1281, 1961.
165. R. Zwanzig, J. Chem. Phys., 38, 1603, 1605, 1963;  
52, 3625, 1970.
166. R.J. Passeron, J. Phys. Chem., 68, 2728, 1964.

167. P. Walden, *Z. Phys. Chem.*, **55**, 207, 1906; **78**, 257, 1912.
168. R. Copal and M.H. Hussain, *J. Ind. Chem. Soc.*, **40**, 981, 1963.
169. L.O. Longsworth, *J. Phys. Chem.*, **67**, 639, 1963.
170. M. Della Monica, U. Laennec and L. Scattore, *J. Phys. Chem.*, **72**, 2124, 1968.
171. G. Broers, *J. Chem. Phys.*, **28**, 1153, 1956.
172. D.G. Miller, *J. Phys. Chem.*, **64**, 1598, 1960.
173. G.J. Mills in *Chemical Physics of Ionic Solutions* pp 571-72, Ed. B.E. Conway and R.O. Baxendale, Wiley, New York, 1966.
174. R.H. Stokes and I.A. Weeks, *Austral. J. Chem.*, **17**, 204, 1964.
175. R.H. Stokes in *The Structure of Electrolytic Solutions*, Ed. N.J. Nener, Wiley, New York, 1959.
176. R.M. Fuoss, *Proc. Natl. Acad. Sci. (U.S.)* **45**, 807, 1959.
177. H.S. Frank in *Chemical Physics of Ionic solutions*, Ed. B.E. Conway and R.O. Baxendale, Wiley, New York, 1966, Chapter 4.
178. G. Atkinson and D.R. Cox, *J. Phys. Chem.*, **69**, 128, 1965.
179. R.L. Key, G.P. Cunningham and D.F. Evans, in *Hydrogen Bonded Solvent Systems*, Ed. A.H. Covington and P. Jones, Taylor and Francis, London, 1965, p. 249.

180. R.L. Kay, B.J. Hales and G.P. Cunningham, *J. Phys. Chem.*, **71**, 3925, 1967.
181. R.L. Kay, C. Sawyski and D.F. Evans, *J. Phys. Chem.*, **69**, 4203, 1965.
182. D.F. Evans and J.L. Broadbater, *J. Phys. Chem.*, **72**, 1037, 1968.
183. M. Spiro in *Physical Chemistry of Organic Solvent Systems*, Ed. A.R. Covington and J. Dickinson, Plenum Press, Chapter 5, Part 3, 1973.
184. R. Fernandez-Prini and G. Atkinson, *J. Phys. Chem.*, **75**, 239, 1971.
185. J.L. Broadbater and R.L. Kay, *J. Phys. Chem.*, **74**, 3803, 1970.
186. P. Singh, Lal Bahadur and N.V. Ramanamurti, *J. Solution Chem.*, **2**, 703, 1973.
187. N.V. Ramanamurti and Lal Bahadur, *Electrochim. Acta*, **25**, 601, 1980.
188. R.L. Kay and J.L. Broadbater, *Electrochim. Acta*, **16**, 667, 1971; *J. Solution Chem.*, **5**, 37, 1976.
189. A.D. Aprano and E.M. Foss, *J. Phys. Chem.*, **67**, 1704, 1722, 1963..

190. P. Hennes, J. Phys. Chem., 78, 907, 1974.
191. J. Hubbard and L. Onsager, J. Chem. Phys., 67, 4850, 1977.
192. N. Islam, M.R. Islam and M. Ahmad, Z. Physik. Chem. (Leipzig) 262, 129, 1981.
193. D.S. Gill, M.S. Chauhan and M.B. Sekhri, J. Chem. Soc. Faraday I, 78, 3451, 1982.
194. D.S. Gill and A.N. Sharma, Indian J. Chem., 21A, 1060, 1982.
195. D.S. Gill and M.B. Sekhri, J. Chem. Soc. Faraday I, 78, 119, 1982.
196. D.S. Gill, A.N. Sharma and H. Schneider, J. Chem. Soc. Faraday I, 78, 465, 1982.
197. R. Kodeja, J. Novak and T. Slama, Ind. J. Chem., 22A, 1029, 1983.
198. (a) R. Iwanobo, Spectrochim. Acta., Part A, 27, 2395, 1971.  
(b) Poda, Fransa et al, Mol. Phys., 27, 521, 1974.
199. (a) K.K. Kundu, A.K. Rakshit and H.N. Das, Electrochim. Acta., 17, 1921, 1972.  
(b) p. Reaking in 'Physico-Chemical Processes in Mixed aqueous solvents', Ed. R. Franks, Heinemann, London (1976), p. 71.  
(c) Kell-Khoo, J. Chem. Soc. (B) 2932 (1971)

200. H. Sadek, Th. P. Tadross and A.-A. Bl-Horakany,  
Electrochim. Acta., 16, 339, 1971.
201. (a) J.B. Desnoyers, Can. J. Chem., 55 (22), 2809, 1977.  
(b) G. Roux, G. Perzosa and J.B. Desnoyers, J. Polym.  
Chem., 17(9), 639, 1979.
202. (a) Kusano, J. Sankaruppan, J. Wadso, J. Chem. Thermod.,  
5, 757, 1973.  
(b) J. Peter Christie, Can. J. Chem., 55, 3700, 1977.  
(c) B.M. Arnott, R.J. Mitchell, T.G.S.R. Murthy,  
J. Am. Chem. Soc., 96, 3875, 1974.
203. (a) S. Terashima, K. Isukita, S. Nakawa, J. Phys. Chem.,  
72, 2345, 1968.  
(b) J.T. Edward, P.G. Farrel and R. Sahidi, J. Chem.  
Soc., Part 1, 73, 705, 1977.
204. R. Cabani and V. Mollica, J. Chem. Soc. Faraday I,  
74, 2667, 1978.
205. E. Renard, C.J. Justice, J. Polym. Chem., 12(9), 633, 1974.
206. C. Peterlinier, P. Lepoitte, Bull. Soc. Chim. Belg., 84,  
1081, 1975.
207. R. Schiavo, R. Acciari, R. Phys. Chem., 102(1-4), 9, 1976.
208. R. Matla, Verh. K. Acad. Wetts. Lett. Schone Kunsten.  
Belg. Klasse, 40, 135, 1978.

209. J.-P. Morel, J. Juillard, D.L. Massart, R. Smits, Anal. Chem., 48, 456, 1976.
210. J. Richard, Redidon, A. Kurt, Kraus (a) J. Chem. Eng. Data, 16, 241, 1971; (b) U.S. Office Saline Water Res. Develop. Progr. Rep. 52-4, No. 695 (1971).
211. V. Vitali, P. Campetti, Chem. Phys., 2(2), 233, 1973.
212. A.D. Pethybridge, H.J. Blandamer and J. Barthel, Proc. 7th Int. Conf. on Non-aq. Solns. I.U.P.A.C. Rosenberg, 11-15 Aug. 1980, p.D-20.
213. N.H. Abraham and J. Missi, J. Chem. Soc. Faraday I, 76, 1219, 1980.
214. A.P. Krushkov, N.T. Smolova, A. Ya. Veveris and B.A. Spivace, Zh. Fiz. Khim., 51(7), 1827, 1977 [Russian Journal of Phys. Chem., 1972, 2, (1977) Eng. J.
215. J.F. Corst in "Solute-Solvent Interactions" — Ed. J.F. Coetzee and C.B. Ritchie, Marcel Dekker, New York (1969) Chapter 8, p. 541.
216. A. Jeans and R. Adams, J. Am. Chem. Soc., 59, 2608, 1937.
217. A.P. Krushkov, "Osnovy Analiticheskoi Khimii (Fundamentals of Analytical Chemistry)" Izd. Khimiya, Moscow (1970) Vol. 5.
218. A.G. Schwartz, J.B. Barker, Talanta, 22(9), 773, 1975.